

Director's Digest

FATS AND PROTEINS RESEARCH FOUNDATION, INC.



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#320

A Demonstration of Fat and Grease as an Industrial Boiler Fuel

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Jointly Funded by:

Poultry Protein & Fat Council of the U.S. Poultry & Egg Association
Fats and Proteins Research Foundation, Inc.
The University of Georgia

A Demonstration of Fat and Grease as Industrial Boiler Fuel

EXECUTIVE SUMMARY

The University of Georgia (UGA) Engineering Outreach Service (EOS) used fats and grease (chicken fat, yellow grease, choice white grease, and beef tallow) as industrial boiler fuels in the 100,000 lb./hr. No. 2 boiler at the UGA steam plant during January and February 2002. The project was funded by the Fats and Proteins Research Foundation, Inc. and the Poultry Protein & Fat Council of the U.S. Poultry & Egg Association. The objectives of the project were to publicly demonstrate the use of biofuel for industrial steam production and to examine the procedures necessary for its use.

Fuel	No. of Tests
Natural Gas	9
Choice White Grease	10
Choice White Grease - Fuel Oil Blend	12
Tallow	13
Tallow Fuel - Oil Blend	15
Yellow Grease - Fuel Oil Blend	19
Yellow Grease	21
No. 2 Fuel Oil	22
Chicken Fat - Fuel Oil Blend	23
Chicken Fat	29
Total	173

Tests were conducted Jan. 28 thru Mar. 15, 2002.

Biofuels, either singly or blended with No. 2 fuel oil, are technically and economically viable alternatives to No. 2 fuel oil. Biofuels are user friendly and less hazardous than petroleum fuels. The addition of biofuel combustion capability is simple and inexpensive. It is not necessary to replace or compromise the operation of existing fossil fuel systems.

Industrial boiler operators can use these results to economically justify the use of biofuels and to support air emissions permit submittals. Even lower emissions levels may be obtained from boilers employing advanced combustion systems.

Summary of Results:

1. Laboratory analyses showed that the fats and greases tested have high heating value, low ash, negligible sulfur, low moisture, and other physical and chemical properties conducive to their use as boiler fuel. Heating values for the biofuel blends tested are within 95% of the heating value of No. 2 fuel oil.

2. The 100,000 lb./hr. No. 2 boiler at the UGA steam plant was retrofitted to burn biofuels for approximately \$31,000, including the cost to add flue gas recirculation (FGR). This amount does not include any expense for the construction of fuel storage facilities, which were not required for the demonstration program. The biofuel heat exchanger was obtained without cost to the project. It was not necessary to replace or modify the boiler fuel train or nozzle for these tests.
3. The tests demonstrated that the biofuels burn cleanly, readily, without odor and without damage to boiler equipment.
4. During this test program, biofuels produced steam within 3.8% to 5.3% of the efficiency of No. 2 fuel oil. Biofuels blended with No. 2 fuel oil were more efficient than unblended biofuels, and can actually produce steam with more efficiency than No. 2 fuel oil. Throughout the tests part load efficiency was greater than maximum load efficiency, and steam production with FGR was more efficient than without FGR.
5. Biofuels are clean burning. They generally produce fewer combustion emissions than No. 2 fuel oil.
6. Flue gas recirculation is an effective way to reduce NO_x emissions for both fossil and biofuels.

Impact of the Research Results relative to the requirements for Boiler No. 2 in the UGA Part 70 Operating (air emissions) Permit (“the Permit”):

1. The Permit prohibits the burning of any fuel whose sulfur content exceeds 1.3% (para. 3.2.1). The maximum sulfur content of any biofuel tested was 0.007%, and 0.13% for any biofuel blended with No. 2 fuel.
2. The Permit limits particulate matter emissions to 0.417 lb/mmBtu (para. 3.4.1). The maximum total particulate (non-condensable and condensable) emission rate of any biofuel was 0.083 lb/mmBtu.
3. The Permit limits visible emissions to 40% opacity (para. 3.4.9). Smokestack opacity ranged between 0% and 11% during the biofuel tests.

Impact of the Research Results relative to the GA Rules for Air Quality Control (the “Rules”):

1. The Rules (Sections (2)(d)2 & 3) limit particulate emissions from all fuel-burning equipment, of any size, to 0.10 lb/mmBtu and opacity to 20%. The maximum total particulate (non-condensable and condensable) emission rate of any biofuel was 0.083 lb/mmBtu. Smokestack opacity ranged between 0% and 11% during the biofuel tests.

2. The Rules (Section (2)(d)4) limit NO_x emissions to 0.3 lb/mmBtu from fuel oil burning equipment, of any size, in an attainment area. The maximum NO_x emission rate of any biofuel tested was 0.23 lb/mmBtu.

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Acknowledgements

This research project was jointly funded by Poultry Protein & Fat Council of the U.S. Poultry & Egg Association, the Fats and Protein Research Foundation, Inc., and The University of Georgia

The University of Georgia (UGA) Engineering Outreach Service (EOS) gratefully acknowledges the support of:

- The test team: Erin Callaghan, Bryan Graffagnini, and Javier Sayago,
- UGA steam plant personnel, in particular: John Benca, Jim Olbrych, Danny Langston, Jerry Bray, Dwight Epps and Doug Pittard,
- UGA Environmental, Health & Safety personnel, in particular, Mike Stover,
- UGA faculty, in particular: Dr. John Goodrum, Dr. Jackie Sellers, and Dr. Keshav Das,
- UGA Physical Plant Plumbing, Sheet Metal, Electrical and Welding Shops,
- American Proteins, Inc., especially: Roger Smith, Kevin Custer, and Gary Bottomley,
- Griffin Industries: Shannon Behimer and Dana Hand,
- The GA Dept. of Natural Resources: Don Holder and Susan Jenkins, and
- The Georgia Environmental Partnership.

1. INTRODUCTION

1.1. History and background, Engineering Outreach Service (EOS)

In 1994, responding to state initiatives to increase the rate of technology transfer out of the University System of Georgia laboratories and into the workplace, The University of Georgia began to offer Engineering Outreach and Public Service to increase the competitiveness of the state's industries. UGA has concentrated on providing to industries on-site services in the areas of research and development, technical and practical assistance, regulatory assistance, energy and water conservation, development of alternative energy, by-product recovery, pollution prevention, bioprocessing, value-added processing, and waste minimization/treatment. These services are being delivered mainly to industries and to municipal and county governments. EOS offered to conduct combustion testing of rendered fats, oils, and grease when it learned of the pioneering work conducted by Roger Smith, Vice President Engineering Services, at American Proteins, Inc.

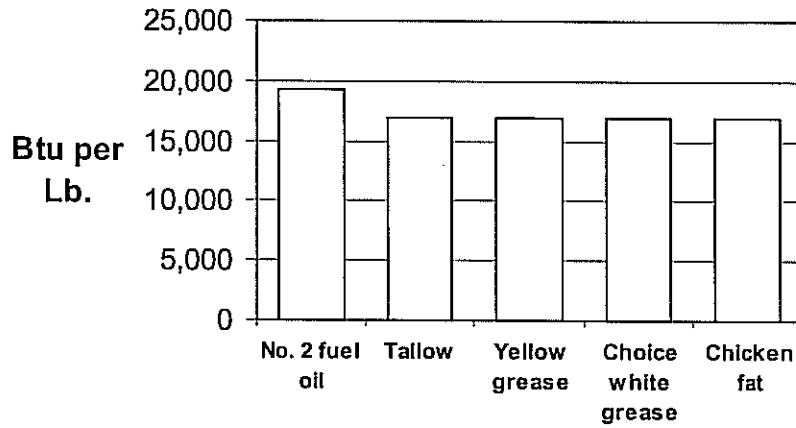
1.2. Project Objectives for *A Demonstration of Chicken Fat as an Industrial Boiler Fuel*:

- Fuel Characterization: Samples of the fats and greases will be laboratory tested to analyze appropriate physical, chemical and combustion characteristics.
- Capital Cost Minimization: The test program will evaluate how to minimize the modifications and resulting capital expense required to convert an industrial boiler to alternative biofuel firing.
- Combustion Tests: Operating and emissions data will be obtained from an industrial boiler fueled with fats and greases, both singly and blended with No. 2 fuel oil.
- Publish results: Technology transfer publication.

1.3. Facts – Fats and Greases

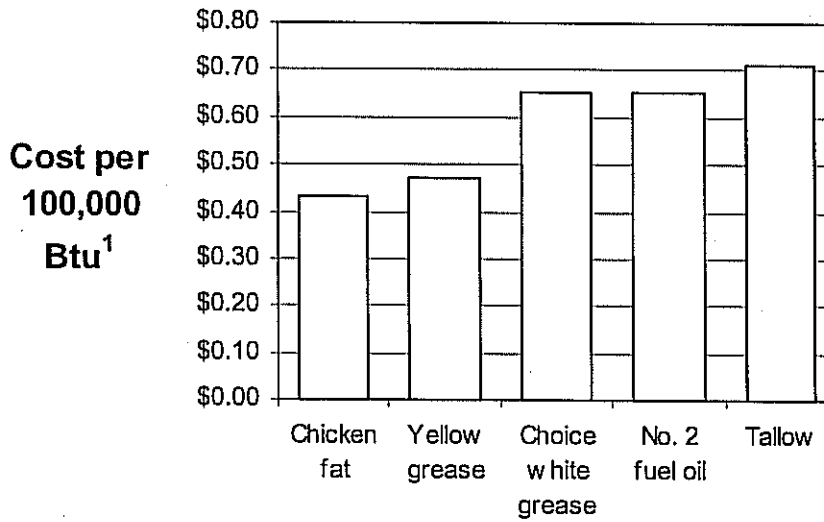
Readily available from meat, poultry and other food-processing operations, chicken fat, yellow grease, choice white grease, and beef tallow were purchased locally. They are competitively priced relative to No. 2 fuel oil, and can represent significant cost savings. The annual production of these biofuels in Georgia alone exceeds 100 million gallons (potentially, over 120 million therms of energy).

Fig. 1. Fuel Energy Content¹



1) PSC Analytical Services, Reading, PA

Fig. 2. Fuel Costs²



1) Costs based upon delivered price to UGA June 2001 and Jan. 2002.

2) PSC Analytical Services, Reading, PA

2. ANALYSIS OF FATS AND GREASE

2.1. Introduction

Laboratory analyses of the fats and grease (biofuel oils) established their commercial specifications relative to standard market product designations. The physical properties of the biofuel oils were used to design the test facility at the UGA central steam plant.

2.2. Sampling Procedures

During the combustion test program, the test team randomly collected three 500-ml samples of each fuel, one each at the beginning, middle and end of each test series. A total of (33) fuel samples were obtained: six (6) samples each of chicken fat and yellow grease; and three (3) samples each of choice white grease, tallow, No. 2 fuel oil and the blends of chicken fat, yellow grease, choice white grease and tallow. (All blends consisted of 33% fat or grease and 67% No. 2 fuel oil.) The team also collected four (4) samples of various solid combustion by-product residues from inside the boiler.

The project procedures maintained sample chain of custody from initial sampling through analysis.

After initial cooling, the test samples were secured in refrigerated storage (4 deg. C.) while at UGA. The test samples were divided into smaller samples for analyses by the UGA laboratories and by commercial laboratories. The samples analyzed by commercial laboratories were overnight shipped in "cold packs".



Fig. 3. Fuel sampling during test

2.3. Fat and Grease Properties

Table 1, Fat and Grease Properties¹				
Test	Chicken Fat	Yellow Grease	Choice White Grease	Tallow
<u>Fatty Acid Profile, % Relative:</u>				
C08:0	<0.10%	<0.10%	<0.10%	<0.10%
C10:0	<0.10%	<0.10%	<0.10%	<0.10%
C11:0	<0.10%	<0.10%	<0.10%	<0.10%
C12:0	<0.10%	<0.10%	<0.10%	<0.10%
C14:0	0.57%	0.70%	1.57%	2.73%
C14:1	0.26%	0.14%	0.36%	0.50%
C15:0	<0.10%	0.11%	0.26%	0.43%
C15:1	<0.10%	<0.10%	<0.10%	0.16%
C16:0	22.76%	14.26%	22.04%	22.99%
C16.1	8.37%	1.43%	5.03%	2.86%
C16.2	<0.10%	<0.10%	<0.10%	<0.10%
C16.3	<0.10%	<0.10%	<0.10%	<0.10%
C16.4	<0.10%	<0.10%	<0.10%	<0.10%
C17:0	0.11%	0.33%	0.63%	1.35%
C17:1	0.12%	0.23%	0.43%	0.75%
C18.0	5.36%	8.23%	9.95%	19.44%
C18.1	42.07%	43.34%	42.45%	41.60%
C18.2	17.14%	26.25%	13.17%	3.91%
C18.3	1.07%	2.51%	0.97%	0.49%
C18.4	0.22%	0.47%	0.29%	0.36%
C20.0	<0.10%	0.33%	0.14%	0.14%
C20.1	0.45%	0.48%	0.56%	0.33%
C20.2	0.20%	<0.10%	0.19%	<0.10%
C20.3	0.19%	<0.10%	0.12%	<0.10%
C20.4	0.45%	<0.10%	0.34%	<0.10%
C20.5	<0.10%	<0.10%	0.11%	<0.10%
C21:5	<0.10%	<0.10%	<0.10%	<0.10%
C22:0	<0.10%	3.50%	<0.10%	<0.10%
C22:1	<0.10%	<0.10%	<0.10%	<0.10%
C22:2	<0.10%	<0.10%	<0.10%	<0.10%
C22:3	<0.10%	<0.10%	<0.10%	<0.10%
C22:4	0.10%	<0.10%	<0.10%	<0.10%
C22:5	<0.10%	<0.10%	0.14%	<0.10%
C22:6	<0.10%	<0.10%	0.22%	<0.10%
C24:0	<0.10%	0.12%	<0.10%	<0.10%
C24:1	<0.10%	<0.10%	<0.10%	<0.10%
unknown components	0.56%	0.72%	1.03%	1.96%
<u>MIU Analysis:</u>				
Moisture & Volatiles	0.12%	0.38%	0.24%	0.17%
Insoluble Impurities	0.08%	0.06%	0.29%	0.12%
Unsaponifiable Matter	0.51%	0.42%	0.73%	0.30%

1) Woodson-Tenent Laboratories, Memphis, TN

To establish the commercial specifications of the fats and greases relative to standard market product designations, Woodson-Tenent Laboratories Division of Eurofins Scientific, Inc., Memphis, TN performed a fatty acid analysis of one sample each of chicken fat, yellow grease, choice white grease and tallow, Table 1. The fatty acid profiles were determined using gas chromatography (AOCS method CE2-66/CE1-620, 0.01% accuracy).

In addition, Woodson-Tenent performed MIU (moisture, impurities, unsaponifiables) analyses of eight (8) biofuel samples, two (2) samples each of chicken fat, yellow grease, choice white grease and tallow, Table 1.

2.4. Viscosity and Specific Gravity

In the summer of 2001, the UGA Biological and Agricultural Engineering (BAE) Department analyzed representative samples of chicken fat and yellow grease, obtained from a local company, to establish a range of viscosity and specific gravity for the design of the test facility.

In the spring of 2002, BAE analyzed fuel samples collected during the test program. The UGA laboratory used a Brookfield LVT viscometer to determine dynamic viscosity (1% accuracy and 0.2% full-scale reproducibility). Specific gravity was measured directly. The dynamic viscosity of each fat and grease, of four (4) biofuel blends and of No. 2 fuel oil was measured over a range of five (5) temperatures and five (5) shear rates. The specific gravity of each fat and grease and of No. 2 fuel oil was measured over a range of five (5) temperatures. One sample of each fuel was tested. All biofuel blends consist of 33% biofuel and 67% No. 2 fuel oil. No. 6 fuel oil viscosity and specific gravity are given below for reference.

Fuel	Dynamic Viscosity, cP	Specific Gravity
No. 2 Fuel Oil ¹	2.3 ^{4,5}	0.83 ⁴
Choice White Grease Blend ¹	4.7 ^{4,5}	not analyzed
Yellow Grease Blend ¹	4.9 ^{4,5}	not analyzed
Tallow Blend ¹	5.2 ^{4,5}	not analyzed
Chicken Fat Blend ¹	12.6 ^{4,5}	not analyzed
Chicken Fat ¹	23.3 ^{4,5}	0.89 ⁴
Yellow Grease ¹	23.3 ^{4,5}	0.89 ⁴
Tallow ¹	24.2 ^{4,5}	0.89 ⁴
Choice White Grease ¹	25.0 ^{4,5}	0.88 ⁴
No. 6 Fuel Oil ²	490 ³	0.97 ³

1) Goodrum et al., 2002; 2) Babcock & Wilcox, 1976; 3) data at 38 deg. C.; 4) data at 54.4 deg. C.; 5) data at 12.94 s⁻¹ shear rate

2.5. Ultimate Analysis and Heating Value

PSC Analytical Services, Reading, PA analyzed a total of (33) biofuel, biofuel/fuel oil blends and fuel oil samples to establish their comparative combustion chemistry and heating values. (All biofuel blends consist of 33% biofuel and 67% No. 2 fuel oil.) PSC used standard ASTM test methods for all analyses. PSC is certified/ accredited by the USEPA, NIOSH, the US Corp of Engineers, and (12) states.

Table 3, Fuel Energy Content and Ultimate Analysis ¹

Fuel	Energy Content, Btu/Lb.	Ash	Carbon	Hydrogen	Nitrogen	Oxygen	Sulfur	Moisture
Chicken Fat	16,873	0.14%	75.3%	11.4%	0.04%	13.1%	0.006%	(trace)
Chicken Fat - Fuel Oil Blend	18,223	0.02%	82.7%	12.2%	0.06%	3.83%	0.12%	(trace)
Yellow Grease	16,899	0.02%	76.4%	11.6%	0.03%	12.1%	0.005%	(trace)
Yellow Grease - F.O. Blend	18,543	0.01%	80.2%	11.6%	0.07%	8.01%	0.13%	(trace)
Choice White Grease	16,893	0.08%	76.5%	11.5%	0.05%	11.6%	0.007%	(trace)
Ch. Wht. Grease - F.O. Blend	18,493	0.01%	82.2%	12.1%	0.09%	5.48%	0.13%	(trace)
Tallow	16,920	0.03%	76.6%	11.9%	0.02%	11.4%	0.003%	(trace)
Tallow Fuel - Oil Blend	18,523	0.06%	80.7%	11.9%	0.01%	7.22%	0.13%	(trace)
No. 2 Fuel Oil	19,237	0.02%	84.0%	11.9%	0.01%	3.78%	0.35%	(trace)

1) PSC Analytical Services, Reading, PA

2.6. General Characterization

The Material Safety Data Sheets (MSDS) included in the Appendix indicate that the fats and greases tested are neither hazardous nor explosive. From the test team's experience, these fats and greases have a distinct and unpleasant odor. However, their volatility is low and the odors do not diffuse readily.

Reports from industry indicate that chicken fat is very miscible in fuel oil and does not readily separate in solution. The test team subjectively confirmed miscibility during the demonstration project; however, definitive data was not collected.

2.7. Discussion

Preliminary laboratory analyses indicated that fats and greases could be used with the No. 2 boiler burner nozzle and that the fuel handing system designed for the test program could easily handle these biofuels. Actual combustion testing demonstrated these findings. Later testing confirmed that biofuels, both singly and blended, have high heating value, low ash, and low sulfur content. Heating values for the biofuel blends tested are within 95% of the heating value of No. 2 fuel oil.

The test team concluded that the chicken fat delivered on January 29, 2002 was substandard; the results from the analyses and combustion of this biofuel were omitted from the report. Initially, the particulate content in the chicken fat caused repeated plugging of the fuel handling system filters. Flue gas testing indicated high levels of NO_x. Subsequent laboratory analyses showed high levels of insoluble impurities.

Two additional deliveries of chicken fat were ordered and tested. Their particulate content was negligible, and the fuel handling system filters did not plug. Insoluble impurity content and emissions of NO_x were consistent with the other biofuels tested. Insoluble impurities were 20% and NO_x emissions were 66% of that from the initial chicken fat delivery. This report includes the findings from the latter chicken fat deliveries.

These results confirm the need for a high degree of filtration for fats and greases delivered as boiler fuel. Inadequately pre-filtered biofuel causes fuel handling problems and may increase gaseous emissions.

PSC Analytical Services reported problems maintaining data consistency due to the lack of homogeneity of the fuel samples they analyzed. The unblended biofuel samples separated into fractions at room temperature. Heating and stirring of the samples is necessary before they can be analyzed.

Research by Dr. John Goodrum at UGA (see References, Section 8) showed that at 40° C chicken fat, yellow grease, choice white grease and tallow were almost entirely solid. Their liquid-solid transition occurs over 40 – 48° C, and they are all completely liquid by approximately 50° C.

All of the samples (biofuels, both singly and blended, and No. 2 fuel oil) examined by Dr. Goodrum exhibited viscosity that transitioned from non-Newtonian to Newtonian. The viscosity of Newtonian fluids does not vary with shear rate. The viscosity of these fuels initially decreased with increasing shear rate (non-Newtonian fluid behavior), followed by viscosity that became independent of shear rate when the shear rate was increased beyond 12.94s⁻¹. In other words, the viscosity curves leveled off (viscosity became fairly constant at a given temperature) once the fluid was in motion.

The blends of chicken fat, yellow grease, choice white grease and tallow with No. 2 fuel oil showed rheological properties very similar to those of pure No. 2 fuel oil.

3. TEST FACILITY DESCRIPTION

3.1. The University of Georgia Steam Plant No. 2 Boiler

All combustion testing was conducted using the No. 2 boiler located at the central steam plant at The University of Georgia campus in Athens, Georgia.

Combustion Engineering, Inc. manufactured this boiler in 1970. It was designed to combust natural gas, No. 2 oil and No. 6 oil for the production of 100,000 lbs./hr. of saturated steam at 250 psig. This boiler currently operates at 100 psig. using natural gas, with No. 2 fuel oil as an alternative.

The No. 2 boiler is a pressurized, water-tube design, package unit. It includes a forced-draft fan and a single steam/air atomized fuel nozzle (Todd Combustion, Inc. TCD Atomizer). The TCD Atomizer nozzle was developed in 1958, and does not include air or fuel staging to reduce NO_x formation. This boiler does not have combustion air preheating or an economizer. Flue gas emissions control is not required.

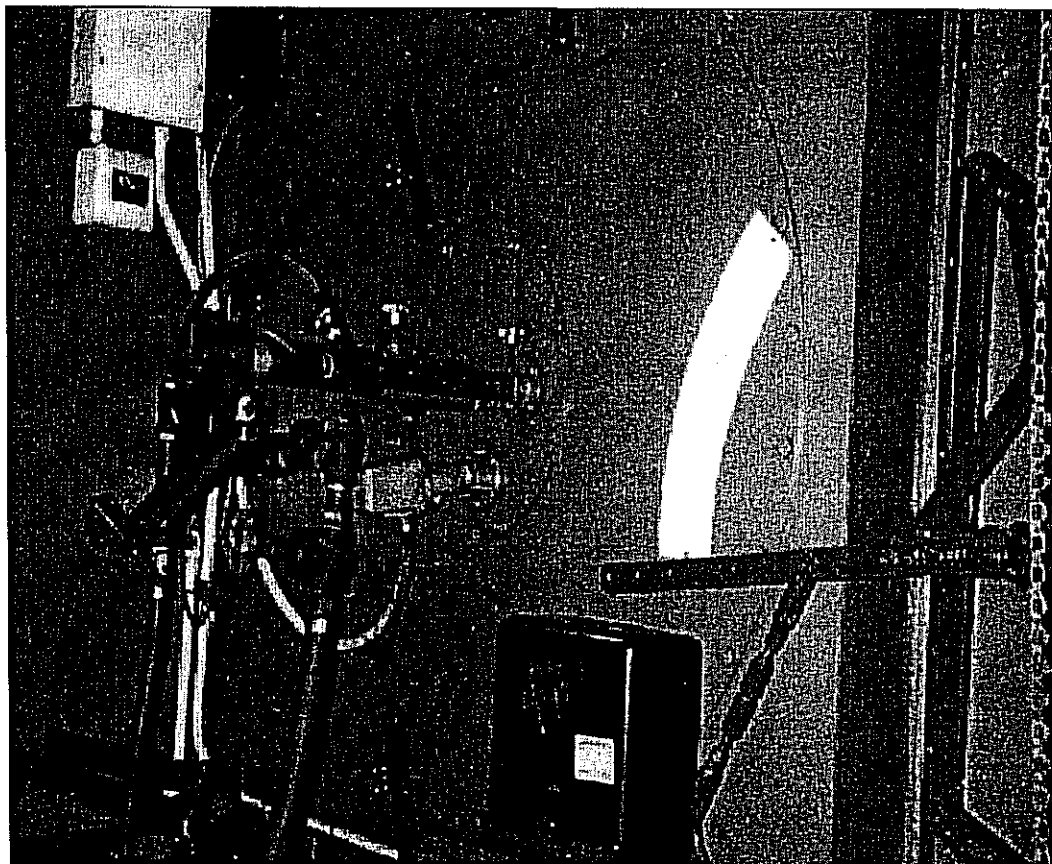


Fig. 4, Burner nozzle for the No. 2 boiler

3.2. Steam Plant Modifications

Neither the boiler burner nozzle nor the fuel train were changed or modified for the combustion tests. The biofuel handling system was piped into the fuel oil delivery piping upstream of the fuel train. For further details, please refer to the Appendix, Dwg. No. SK-001, *Central Steam Plant Site Plan*, and Dwg. No. SK-002, *Boiler No. 2 Process Flow Diagram*.

A 7 hp gear pump supplied biofuel to the boiler fuel train at a maximum of 22 gpm. A pressure control valve and a safety relief valve maintained the pump discharge pressure to a maximum of 275 psig. Two (2) cast iron basket strainers in parallel protected the pump. A shell and tube heat exchanger, which maintained biofuel temperature, was rated for 150 psig and was installed on the gear pump suction side. 1-1/2" dia. carbon steel sch. 40 piping and 300-lb. malleable iron screwed fittings were used throughout. Some sections of the piping were steam traced.

The biofuel delivery system was manually controlled. Instrumentation consisted of two (2) fuel flow meters, a rotary flow indicator, and necessary pressure and temperature gauges.

The only modification to the boiler was the temporary addition of a flue gas recirculation (FGR) duct and damper. No modifications were made to either the boiler internals or instrumentation.

3.3. Fuel Handling System

The biofuel handling system consisted of both mobile equipment and equipment temporarily installed for the tests. Biofuels were transported to the University and stored on site in a 7,000 gallon tanker-trailer. A second tanker trailer was utilized for biofuel/ fuel oil batch mixing. The test protocols were planned so that the quantity of biofuel available at the beginning of each testing period was sufficient for the completion of that test, thus avoiding the complexity of changing fuel supply during a test.

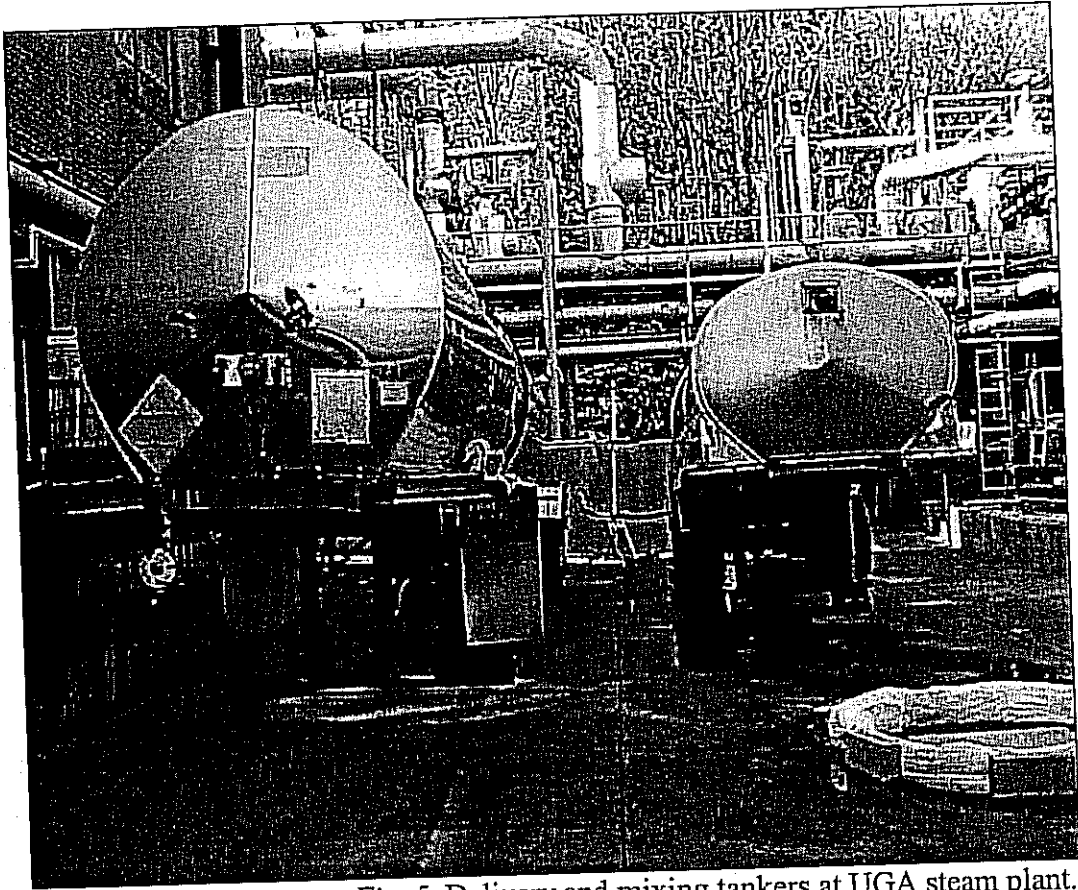


Fig. 5, Delivery and mixing tankers at UGA steam plant.

Previous industrial experience had indicated that after a 24 hour exposure to extreme winter ambient temperatures, a 7,000 gallon tanker load of biofuel could become too viscous for handling. Therefore, all biofuel was delivered warm (over 100° F) and within 4 hours after loading. All biofuel suppliers were located near Atlanta, GA, less than 80 miles from the steam plant. Delivery tankers were piped to the fuel system immediately after they arrived at the UGA steam plant. The fuel system continuously recirculated the biofuel to the tanker and kept it warm and mixed.

A heat exchanger was included in the fuel handling system prior to fuel transfer to the boiler. The heat exchanger maintained the biofuel temperature to approximately 165° F to reduce its viscosity to that of No. 2 fuel oil. The source of heat for this unit was 5 psig steam.

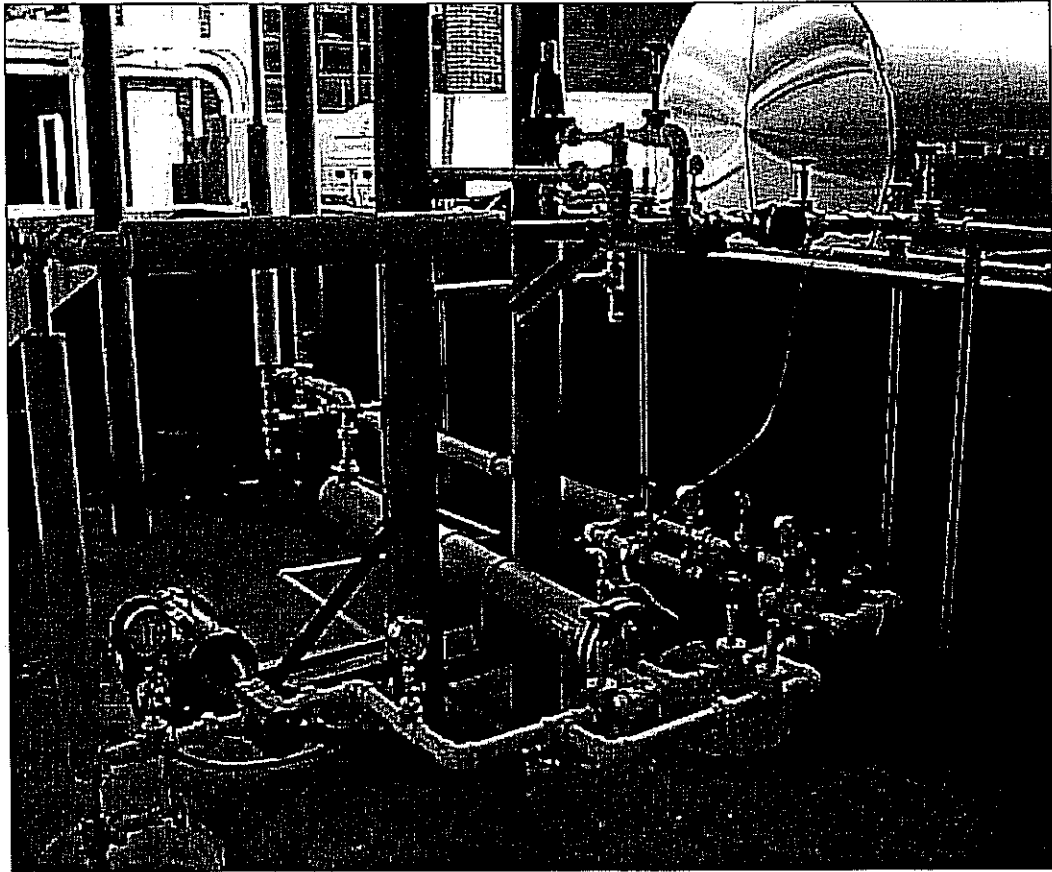


Fig. 6, Fuel heating, pumping and mixing system.

3.4. Flue Gas Recirculation System

The FGR system consisted of a 20 inch diameter duct connecting the boiler flue gas breaching (at 0.0 in. wg. static pressure) and the forced draft fan inlet (at negative 0.25 in. wg. static pressure). An adjustable butterfly damper was installed in the duct to control flow. Pitot tube flow measurements indicated that 7 to 10% of the flue gas exiting the boiler was recirculated back into the burner.

3.5. Environmental Protection

Provisions were made to maintain personnel safety and to avoid and control spills in accordance with the UGA Spill Prevention Control and Countermeasure Plan (SPCCP) and the UGA Storm Water Pollution Prevention Plan (SWPPP). The biofuel transfer pump, two fuel strainers, and the heat exchanger were located in a diked containment area to isolate them from the sanitary sewer system.

4. COMBUSTION DEMONSTRATION

4.1. Introduction

Industrial boiler operating experience and data were obtained while firing natural gas, No. 2 fuel oil, biofuels, and biofuels blended with No. 2 fuel oil. Baseline combustion testing was conducted by firing natural gas and fuel oil. Testing was conducted both with and without flue gas recirculation and with a range of boiler loads to evaluate emissions and combustion efficiencies under a wide range of operating conditions. The tests demonstrated that the biofuels burn efficiently, cleanly, readily, without odor and without damage to boiler equipment.

4.2. Test Schedule

The University of Georgia in Athens, GA is subject to mild winter conditions and considers the winter heating season to extend from late November to mid-February. Steam demand on the central steam plant is in the 100,000 to 200,000 lb/hr range during the winter heating season. This demand reduces to less than 50,000 lb/hr during the summer. Throughout the year, daily load peaks in the early morning.

The project team scheduled the tests during the winter heating season to allow for testing of the No. 2 boiler at maximum load. The tests began January 28, 2002 and continued daily for three weeks until February 15, 2002. Maximum load tests were conducted in the morning, part load tests in the afternoon. A follow-up test on chicken fat was conducted on March 15, 2002.

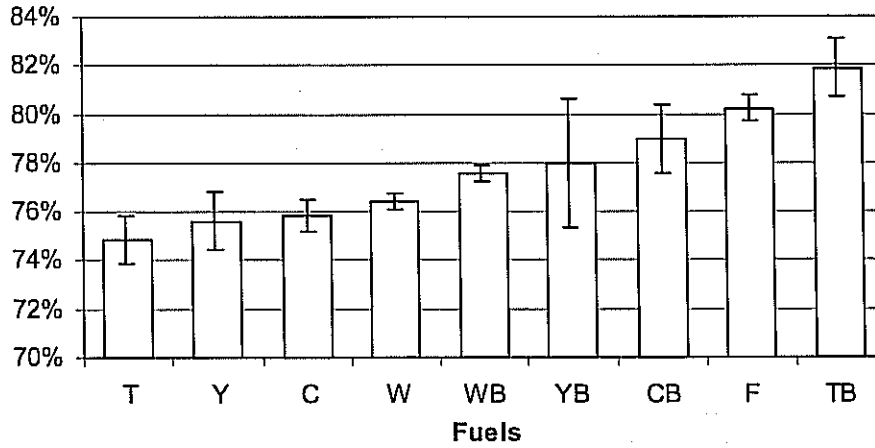
In general, the sequence of the testing was chicken fat and blend, yellow grease, choice white grease and blend, tallow, yellow grease blend and tallow blend. All blends consisted of 33% fat or grease and 67% No. 2 fuel oil. Natural gas and No. 2 fuel oil testing was conducted periodically throughout the test period.

4.3. Boiler Efficiency

Boiler efficiency is calculated as boiler steam energy output (btu/hr), less feedwater energy input, as a percentage of boiler fuel energy input (btu/hr). Steam plant instrumentation measured the flow (lb/hr) and pressure (psig) of the saturated steam produced by the boiler. Feedwater energy input was based on the temperature at the deaerator.

Fuel energy input is the product of the flowrate and the energy content of the fuel. The flowrate was determined from the flow at the boiler burner nozzle flowmeter divided by the time interval between meter readings. PSC Analytical Services analyzed samples of each fuel to determine specific energy content.

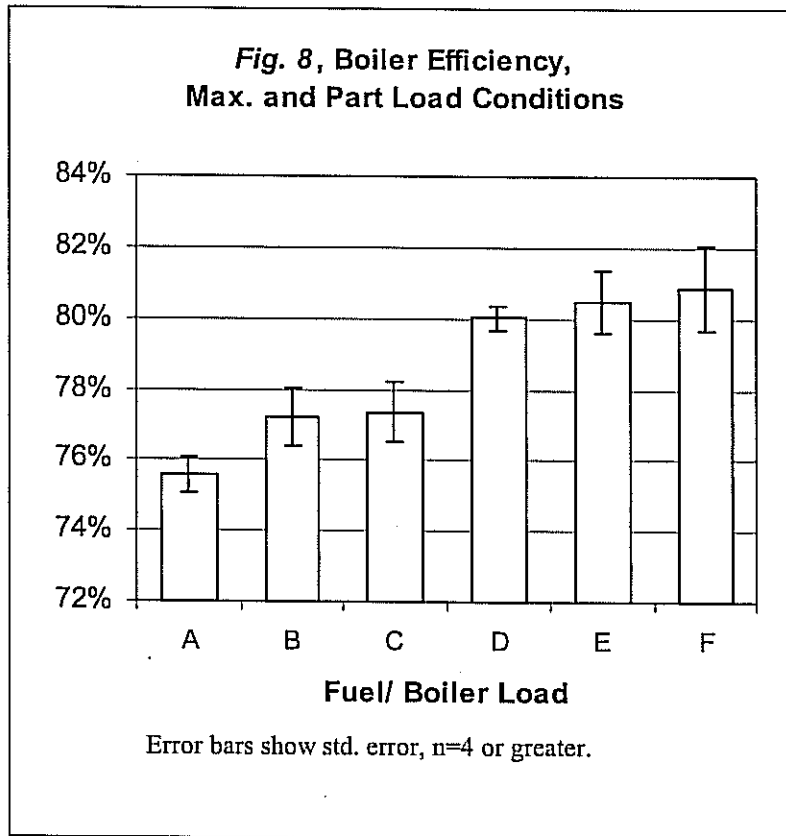
**Fig. 7, Boiler Efficiency,
Biofuels and Fuel Oil**



- 1) Max. and part load conditions are averaged.
- 2) Error bars show std. error, n=4 or greater.

Fuel Abrev.	Average Efficiency	Fuels
T	74.9%	TALLOW
Y	75.6%	YELLOW GREASE
C	75.9%	CHICKEN FAT
W	76.4%	CHOICE WHITE GREASE
WB	77.6%	CHOICE WHITE GREASE - FUEL OIL BLEND
YB	78.0%	YELLOW GREASE - FUEL OIL BLEND
CB	79.0%	CHICKEN FAT - FUEL OIL BLEND
F	80.2%	No. 2 FUEL OIL
TB	81.9%	TALLOW - FUEL OIL BLEND

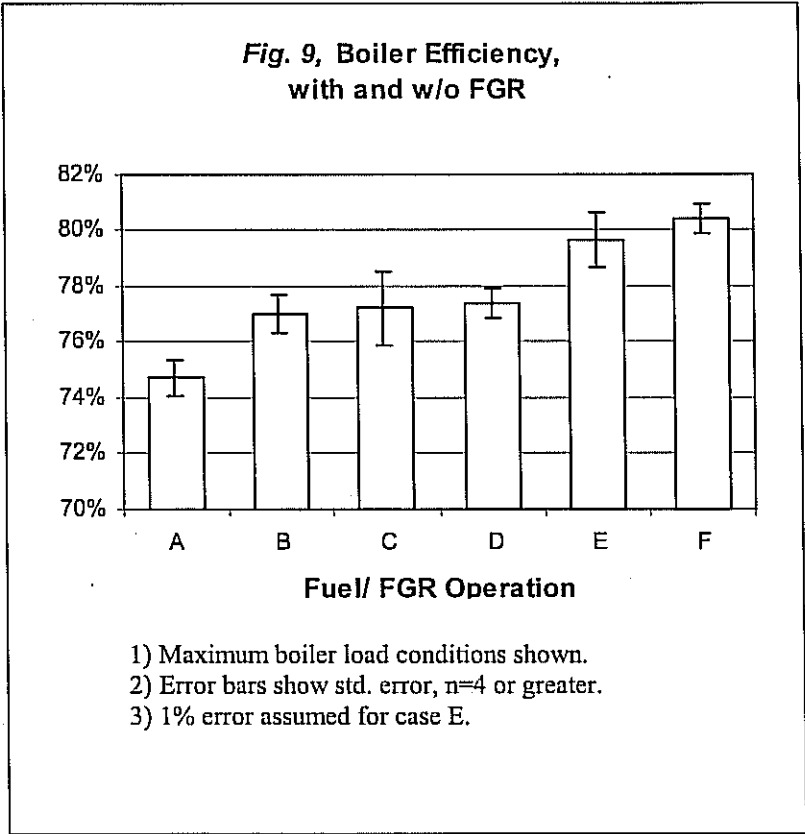
Fig. 7, Legend



Fuel/ Load	Average Efficiency	Fuel & Boiler Loading
A	75.6%	BIOFUELS @ MAX. LOAD
B	77.2%	BIOFUELS @ PART LOAD
C	77.4%	BLENDED BIOFUELS @ MAX. LOAD
D	80.0%	No. 2 FUEL OIL @ MAX. LOAD
E	80.5%	No. 2 FUEL OIL @ PART LOAD
F	80.9%	BLENDED BIOFUELS @ PART LOAD

Fig. 8, Legend

There was no significant difference in boiler efficiency when using 100% #2 fuel oil and blends with 33% biofuel oil according to a Student's t-test at the $\alpha = 0.05$ significance level. Boiler efficiency of #2 fuel oil was significantly higher compared to biofuel oil alone. Boiler efficiency was significantly higher using tallow blend compared to #2 fuel oil under half load conditions.



Fuel/ FGR. Operation	Average Efficiency	Flue Gas Recirculation (FGR) Status
A	74.7%	BIOFUELS, w/o FGR
B	77.0%	BIOFUELS with FGR
C	77.2%	BLENDED BIOFUELS w/o FGR
D	77.4%	BLENDED BIOFUELS with FGR
E	79.6%	No. 2 FUEL OIL w/o FGR
F	80.4%	No. 2 FUEL OIL with FGR

Fig. 9, Legend

4.4. Combustion Characteristics

The steam plant did not experience any unusual operating problems while burning biofuel or biofuel blends. The boiler lit off quickly and ran quietly. There were no fat and grease odors in the plant.

Observations through the furnace sight glasses indicated that biofuels generally burn with a flame that is more yellow-colored and widely dispersed than with either natural gas or No. 2 fuel oil. However, the flame pattern was well contained within the furnace, as was verified by later internal inspection of the furnace.

At maximum load, fuel pressure to the boiler nozzle averaged 160 psig for unblended biofuels, 157 psig for blended biofuels, and 119 psig for No. 2 fuel oil. Atomizing steam pressure averaged 97 psig under all conditions.

A thermocouple was installed in the furnace to measure its internal temperature. The thermocouple projected approximately 3 ft. into the back of the furnace, at the flue gas backpass. Temperature readings were read from a handheld digital thermometer.

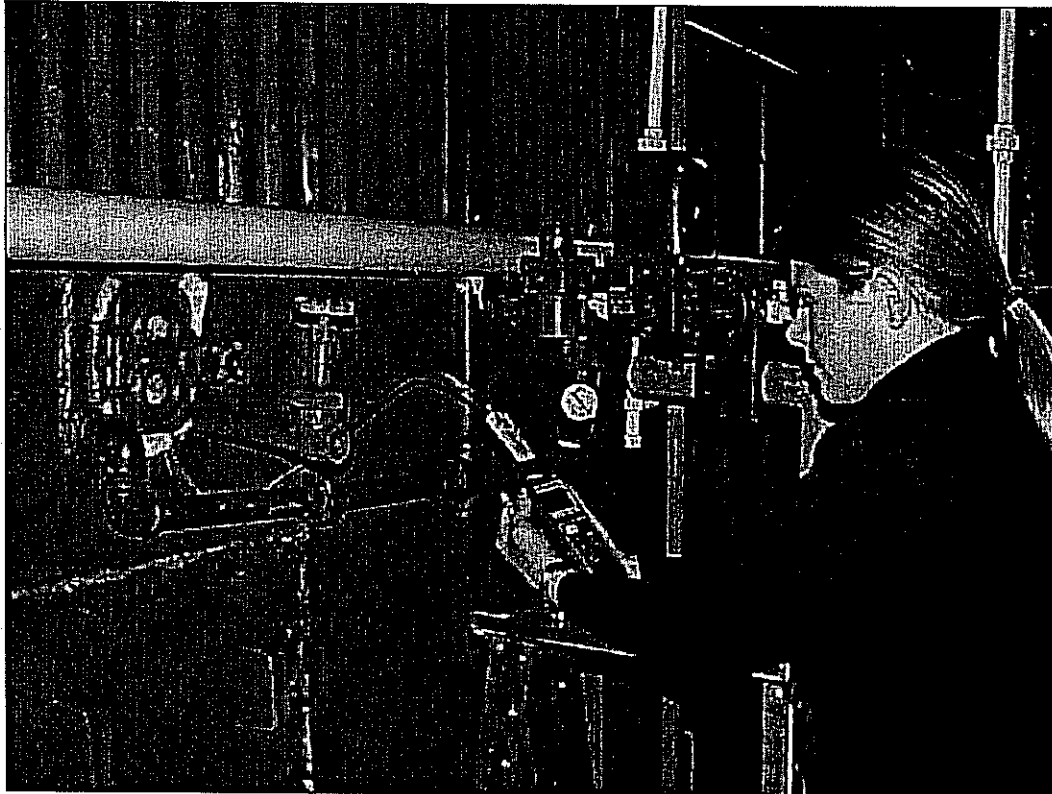


Fig. 10, Furnace temperature measurement system

4.5. Inspection of Boiler Internals

The test team inspected the interior of the boiler after several months of firing natural gas exclusively; then, after firing No. 2 fuel oil exclusively; and, finally, after three weeks of biofuel combustion testing. The test team observed that the water tube exterior surfaces were clean and soot-free after natural gas firing. The tube surfaces were soot-covered, black-colored, and somewhat greasy after firing with No. 2 fuel oil.

Following biofuel burning, the interior of the furnace appeared to be almost as clean as it was after firing natural gas, and much cleaner than it was after burning No. 2 fuel oil. A slight blackening of the tube surfaces, following the flame pattern, was observed in the front half of the 25-ft. long furnace.

A scattering of baked-on solid deposits (each approximately 2-3 mm in diameter) was found on the tube surfaces in the back half of the furnace. The UGA Chemical Analysis Laboratory analyzed three (3) samples of this material with an ICP mass spectrometer and found that they consist predominately of the elements Fe, Na, P, K, and Ca.

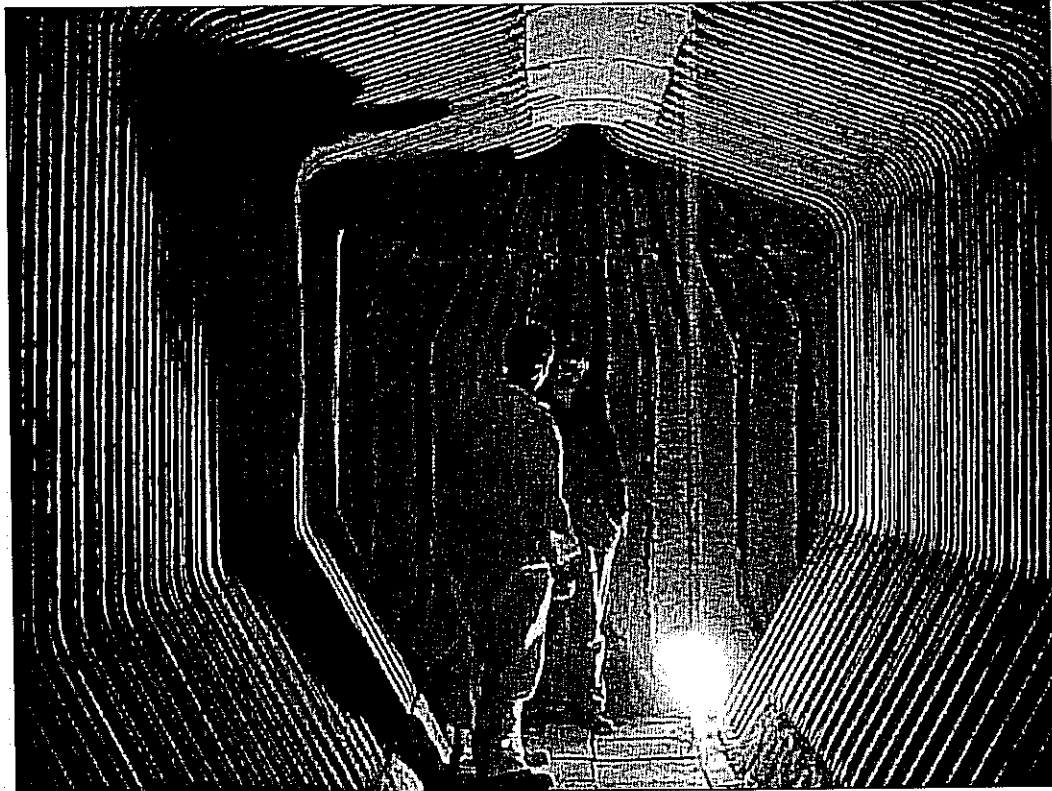


Fig. 11, Inspection of boiler heat transfer surfaces after testing biofuels

4.6. Discussion

The standard error calculated for the efficiency data ranged from 0.3% to 1.4%, plus or minus, with one data point showing a 2.6% +/- standard error, $n = 4$. The instrumentation used is standard industrial class equipment, and was not specially calibrated for this test. The greatest potential for error is the time recording taken between fuel meter readings. A time interval of 13 minutes was the minimum used. All time readings were taken with a wristwatch to the nearest minute.

There was no significant difference in efficiency under part load conditions versus full load according to an unpaired Student's t-test at the $\alpha = 0.05$ significance level. Also, there was no significant difference in efficiency with or without FGR. However, combustion with FGR resulted in significantly less excess air in the flue gas and indicates more complete combustion and less loss of energy to the stack.

5. EMISSIONS TESTING

5.1. Particulate Testing

Advanced Air Consultants Inc. (AAC), Murrayville, GA performed emissions tests for condensible (both organic and inorganic) and non-condensable particulate. Two test runs, each one hour long and conducted under normal boiler operation, were performed on each of five different fuels (chicken fat, yellow grease, choice white grease, tallow, and No. 2 fuel oil). Simultaneously with the particulate tests, the UGA Engineering Outreach test team measured gaseous emissions.

AAC conducted all particulate testing according to the reference methods developed by the US EPA and promulgated in the Code of Federal Regulations, Title 40, Parts 51 and 60. AAC is certified per NELAC procedures to perform EPA Method 5 particulate measurement. All of the test equipment was manufactured and calibrated as specified in the EPA methods.

The particulate testing location was in a straight section of the No. 2 boiler breaching, between the boiler and a combined boiler stack. The number of velocity traverse points was chosen based on the distance of the test ports from up and downstream flow disturbances. Flow disturbances were located 2.5 diameters upstream and 1.0 diameters downstream from the test ports. Twenty traverse points were sampled.

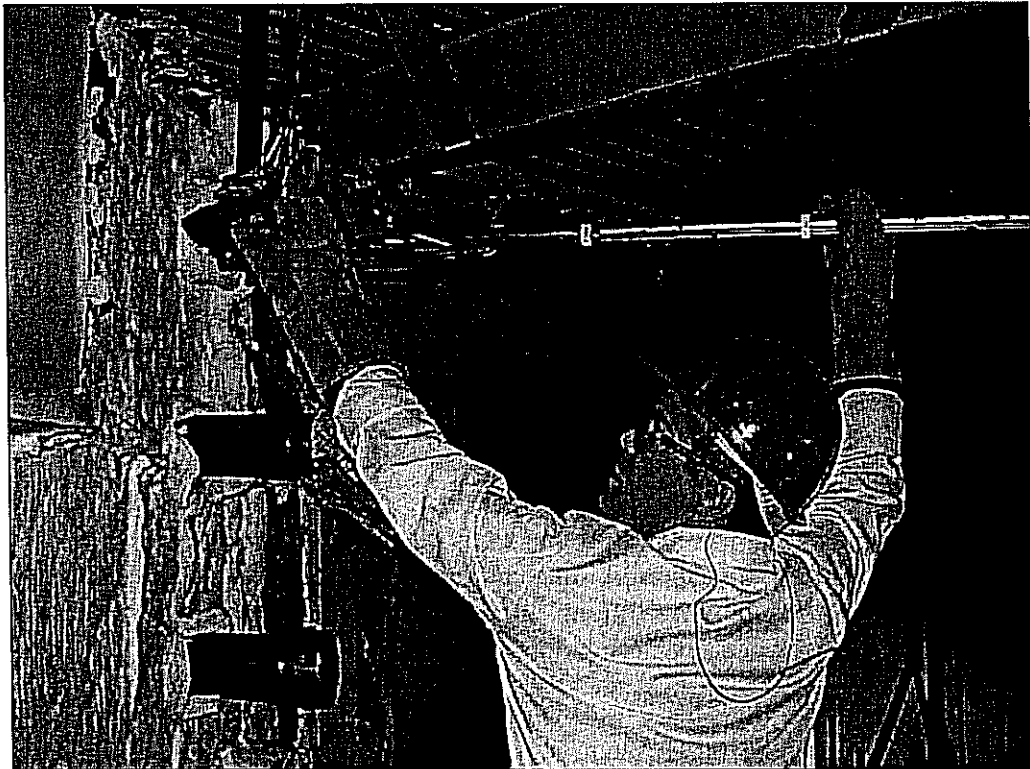


Fig. 12. Inserting particulate testing probe into breaching.

AAC used a sampling train consisting of a stainless steel nozzle, stainless steel union, stainless steel lined probe, glass filter holder with Teflon filter support, four glass impingers, umbilical cord, vacuum pump, dry gas meter and orifice. Both the probe and filter compartment were heated to 250 deg. F. The impingers were placed in an ice bath to remove moisture from the sample gas stream. A "S" type pitot tube and an inclined manometer measured the gas velocity pressures. A type K thermocouple and a digital thermometer measured the gas temperature. The Denver Instruments Model A-250 analytical balance in the AAC laboratory weighed the particulate samples.

In accordance with US EPA Method 19 (40CFR60), AAC calculated fuel F-Factors using the fuel analysis data presented in Section 3 of this report. F-Factors are used to calculate emission rates in pounds per million Btu, per US EPA methodology.

The US EPA "F Factor" technique is a more convenient method to determine emissions on a mass per unit heat input basis. This technique allows the calculation of emissions without the need for precise measurement of fuel flow and combustion efficiency.

Fuel	F-Factor, Fd
Chicken Fat	8,865
Yellow Grease	9,108
Choice White Grease	9,145
Tallow	9,179
No. 2 Fuel Oil	8,850

Source: Advanced Air Consultants, Inc., Murrayville, GA

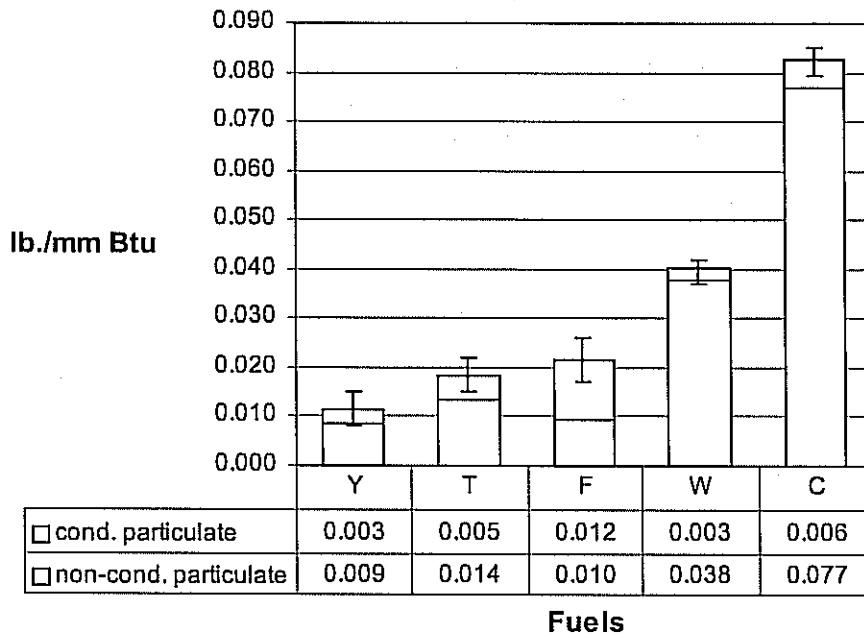
Fd is the ratio of the quantity of dry effluent gas generated by combustion to the gross calorific value of the fuel, dscf/10⁶Btu.

Ref.: *Federal Register*, 40:194, Part V, Oct. 6, 1975,

AAC also monitored smokestack opacity. Maximum opacity with chicken fat was 4% and yellow grease was 6%. There was no opacity observed while burning tallow. Opacity was not monitored while burning choice white grease.

Opacity testing was not performed in strict accordance with GA EPD compliance regulations, which require an average value for a series of opacity observations over a one-hour period. Instead, opacity testing during the program consisted of a series of spot observations. However, all opacity readings were taken by GA EPD-certified opacity readers.

**Fig. 13, Particulate Emissions,
Biofuels and Fuel Oil**



- 1) Test conditions: maximum boiler load with FGR.
- 2) Condensable particulate = organic + inorganic condensable particulate.
- 3) Total particulate = non-cond. + cond. particulate.
- 4) Error bars show std. error for total particulate.

Fuel Abrev.	Fuel
Y	YELLOW GREASE
T	TALLOW
F	No. 2 FUEL OIL
W	CHOICE WHITE GREASE
C	CHICKEN FAT

Fig. 13. Legend

5.2. Gaseous Emissions Testing

The UGA Engineering Outreach team used an ENERAC 3000E analyzer to measure the gaseous emissions from the No. 2 boiler. The team recorded both average and instantaneous measurements of flue gas concentrations for oxygen, carbon monoxide, carbon dioxide, combustible gases, excess air, nitric oxide, nitrogen dioxide, NO_x (NO + NO₂), and sulfur dioxide. The analyzer software

program enabled the recording of emissions data directly to a spreadsheet file on the hard drive of a laptop computer. Data was recorded during steady state operations for each fuel tested, at both maximum and part loads and at each FGR damper setting.

The ENERAC 3000 portable emissions analyzer is a self-contained, extractive flue gas monitoring system utilizing electrochemical sensors with an internal sample pump designed for 600-900 cc/minute. A separate vacuum pump extracted flue gas from a breaching port and discharged it to the ENERAC. Teflon tubing interconnected a filter probe in the breaching through two moisture condensers to the vacuum pump and then to the analyzer.

The ENERAC sensors use an electronically controlled circuit to minimize zero drift and reject cross interference from other compounds, in compliance with EPA Conditional Test Methods (CTM) -022, -030 and -034. The performance specifications of the CTM-022 method are equivalent to US EPA Method 7E requirements. The accuracy of the sensors is +/-2%, and they are capable of operating at 1.5 orders of magnitude of gas concentrations.

Equipment was calibrated several times per week, and was checked daily for accuracy. The system was allowed to autozero daily. Span calibration of CO, NO, SO, NO₂ was performed 2-3 times per week using calibrated gases (CO at 78 ppm, NO at 124 ppm, SO₂ at 25 ppm, and NO₂ at 92 ppm.)

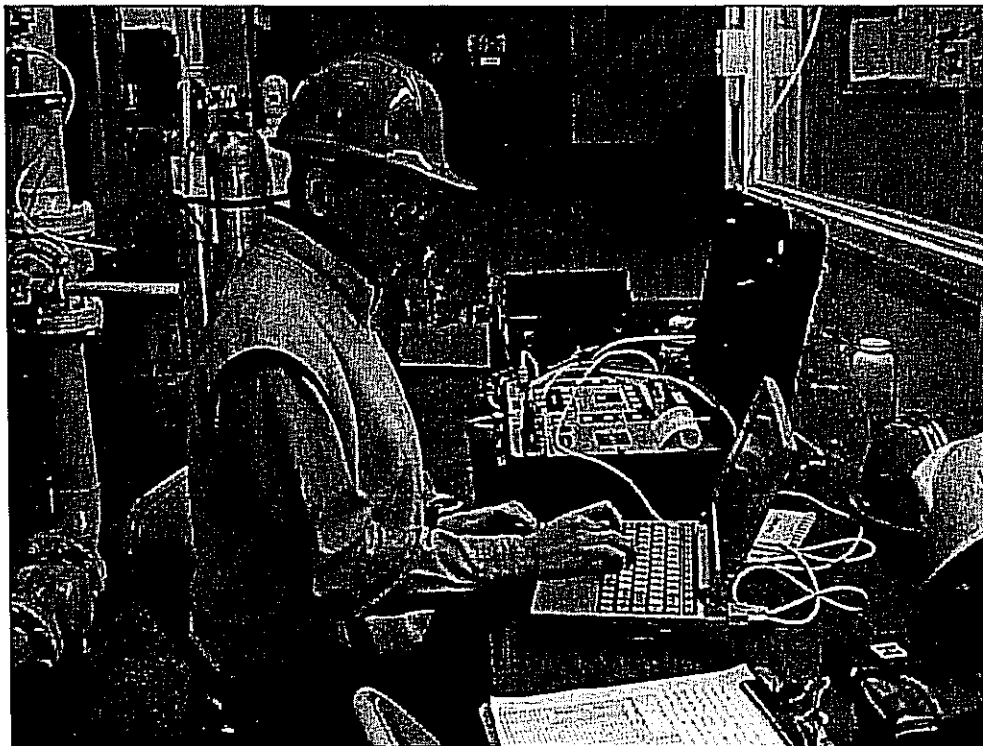
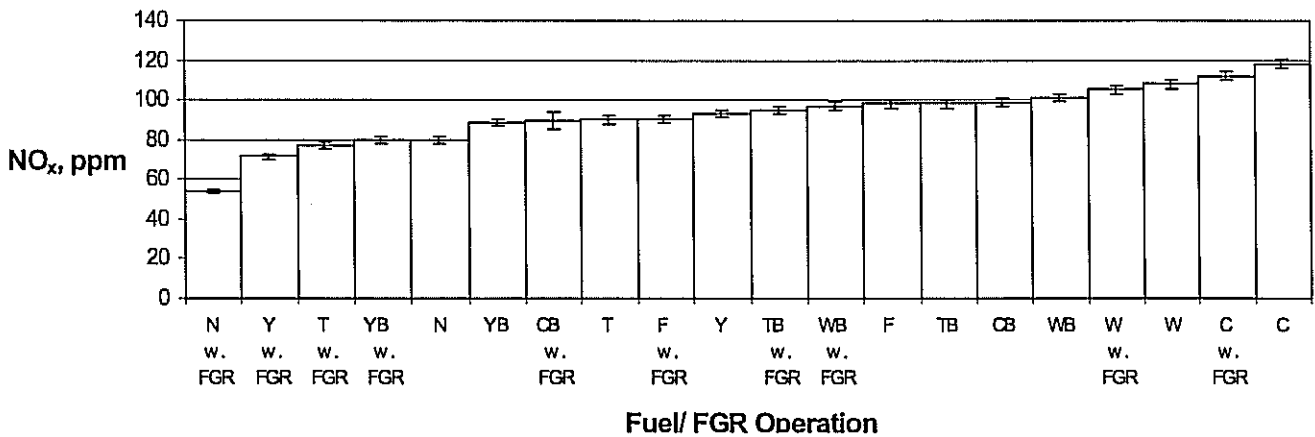


Fig. 14. Logging of emissions data from Enerac 3000E.

Fig. 15, NO_x Emissions

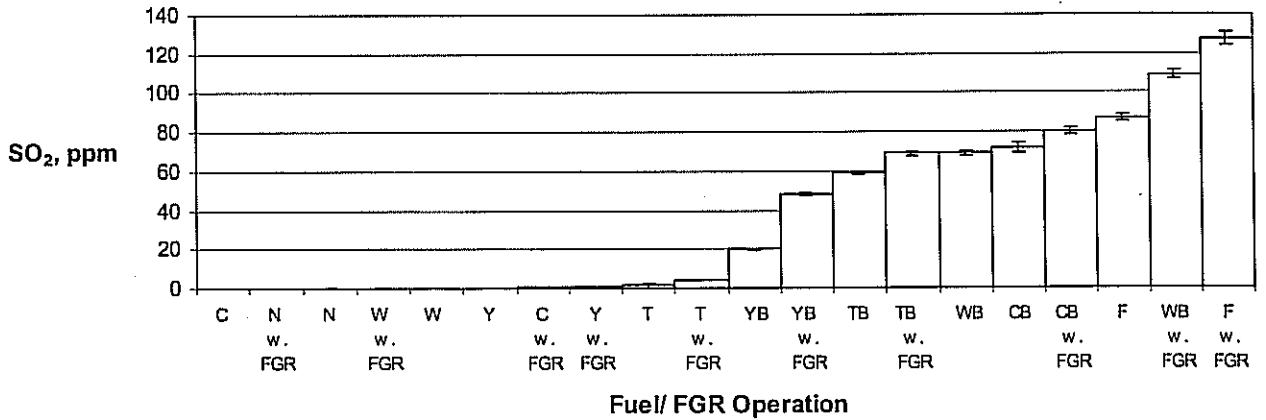


- 1) All tests were conducted at maximum boiler load.
- 2) Error bars show std. error calculated for cases: CB with FGR (n=2) and T w/o FGR (n=3). 2% error assumed for all of the other cases.

Fuel	Legend	NOx emissions, ppm			Furnace Temperature, deg. F.		
		w/o FGR	w. FGR	% reduction	w/o FGR	w. FGR	delta
N	NATURAL GAS	80	54	32.5%	1,983	2,010	27
Y	YELLOW GREASE	93	71	23.7%	1,755	1,830	75
T	TALLOW	90	77	14.4%	1,824	1,928	104
YB	YELLOW GREASE - FUEL OIL BLEND	89	80	10.1%	1,773	1,811	38
CB	CHICKEN FAT - FUEL OIL BLEND	99	90	9.1%	1,756	1,843	87
F	No. 2 FUEL OIL	98	91	7.1%	1,836	1,901	65
TB	TALLOW - FUEL OIL BLEND	98	95	3.1%	1,714	1,790	76
WB	CHOICE WHITE GREASE - FUEL OIL BLEND	101	97	4.0%	1,860	1,954	94
W	CHOICE WHITE GREASE	108	105	2.8%	1,855	1,886	31
C	CHICKEN FAT	118	112	5.1%	1,776	n.a.	n.a.

Fig. 15. Legend

Fig. 16, SO₂ Emissions

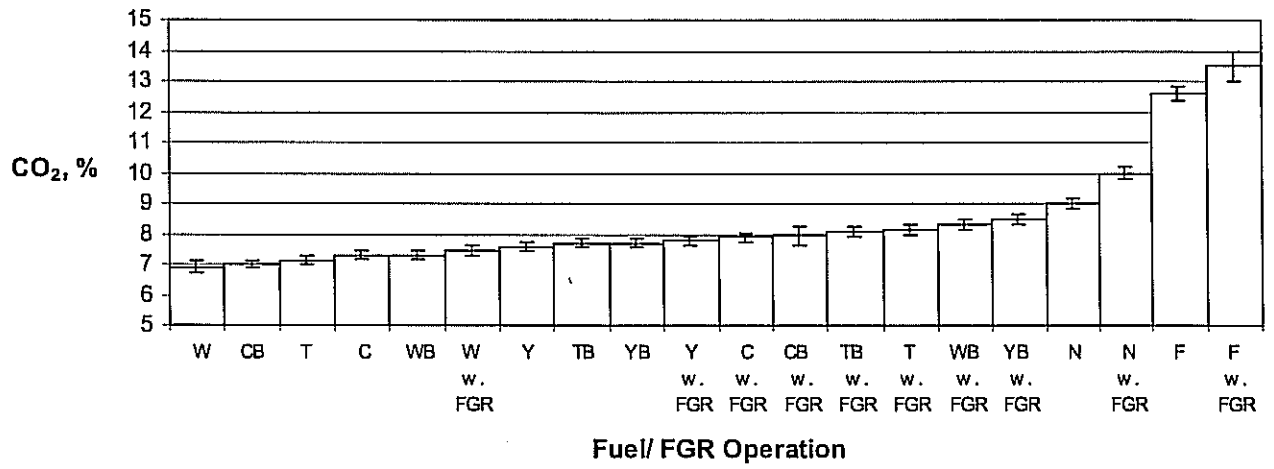


- 1) All tests were conducted at maximum boiler load.
- 2) Error bars show std. error (n=2 or greater) calculated for cases: Y, YB, F, W, and C with FGR; and cases T, CB and W w/o FGR. 2% error assumed for all of the other cases.

Fuel	Legend	SO ₂ emissions, ppm		
		w/o FGR	w. FGR	delta
N	NATURAL GAS	0	0	0
Y	YELLOW GREASE	0	1	1
W	CHOICE WHITE GREASE	0	0	0
C	CHICKEN FAT	0	0	0
T	TALLOW	1	4	3
YB	YELLOW GREASE - FUEL OIL BLEND	20	48	28
TB	TALLOW - FUEL OIL BLEND	59	69	10
WB	CHOICE WHITE GREASE - FUEL OIL BLEND	69	109	40
CB	CHICKEN FAT - FUEL OIL BLEND	72	80	8
F	No. 2 FUEL OIL	87	127	40

Fig. 16. Legend

Fig. 17, CO₂ Emissions

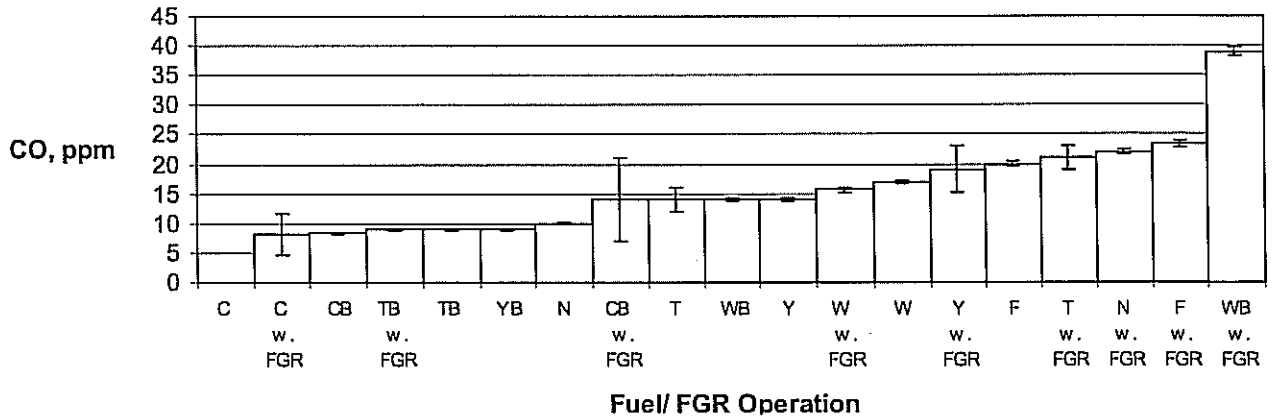


- 1) All tests were conducted at maximum boiler load.
- 2) Error bars show std. error (n=2 or greater) calculated for cases: CB, F, and W with FGR, and T and W w/o FGR.
- 3) 2% error assumed for all of the other cases.

Fuel	Legend	CO ₂ emissions, %		
		w/o FGR	w. FGR	delta
W	CHOICE WHITE GREASE	6.9	7.5	0.6
CB	CHICKEN FAT - FUEL OIL BLEND	7.0	8.0	1.0
T	TALLOW	7.1	8.2	1.1
C	CHICKEN FAT	7.3	7.9	0.6
WB	CHOICE WHITE GREASE - FUEL OIL BLEND	7.3	8.3	1.0
Y	YELLOW GREASE	7.6	7.8	0.2
TB	TALLOW - FUEL OIL BLEND	7.7	8.1	0.4
YB	YELLOW GREASE - FUEL OIL BLEND	7.7	8.5	0.8
N	NATURAL GAS	9.0	10.0	1.0
F	No. 2 FUEL OIL	12.6	13.5	0.9

Fig. 17. Legend

Fig. 18, CO Emissions

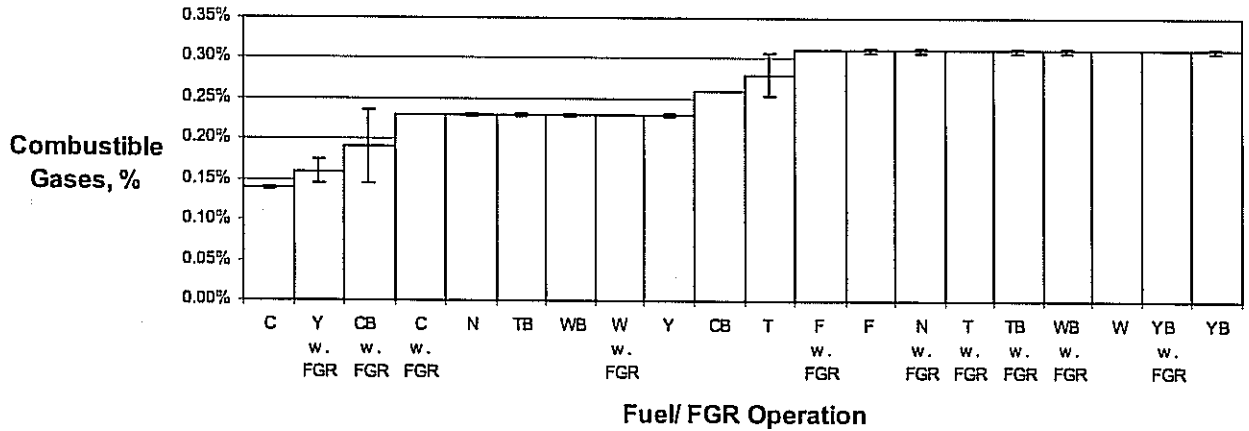


- 1) All tests were conducted at maximum boiler load.
- 2) Error bars show std. error (n=2 or greater) calculated for cases: Y, T, CB, F, W, and C with FGR, and T w/o FGR. 2% error assumed for all of the other cases.

Fuel	Legend	CO emissions, ppm		
		w/o FGR	w. FGR	delta
C	CHICKEN FAT	0	8	8
CB	CHICKEN FAT - FUEL OIL BLEND	8	14	6
TB	TALLOW - FUEL OIL BLEND	9	9	0
YB	YELLOW GREASE - FUEL OIL BLEND	not available		
N	NATURAL GAS	10	22	12
T	TALLOW	14	21	7
WB	CHOICE WHITE GREASE - FUEL OIL BLEND	14	39	25
Y	YELLOW GREASE	14	19	5
W	CHOICE WHITE GREASE	17	16	-1
F	No. 2 FUEL OIL	20	23	3

Fig. 18. Legend

Fig. 19 , Combustibles in Flue Gas



- 1) All tests were conducted at maximum boiler load.
- 2) Error bars show std. error (n=2 or greater) calculated for cases: Y, T, YB, CB, F, W, and C with FGR; and cases T, CB and W w/o FGR.
- 3) 2% error assumed for all of the other cases.

Legend	Combustibles in Flue Gas, %		
	w/o FGR	w. FGR	delta
CHICKEN FAT	0.14%	0.23%	0.09%
NATURAL GAS	0.23%	0.31%	0.08%
TALLOW - FUEL OIL BLEND	0.23%	0.31%	0.08%
CHOICE WHITE GREASE - FUEL OIL BLEND	0.23%	0.31%	0.08%
YELLOW GREASE	0.23%	0.16%	-0.07%
CHICKEN FAT - FUEL OIL BLEND	0.26%	0.19%	-0.07%
TALLOW	0.28%	0.31%	0.03%
No. 2 FUEL OIL	0.31%	0.31%	0.00%
CHOICE WHITE GREASE	0.31%	0.23%	-0.08%
YELLOW GREASE - FUEL OIL BLEND	0.31%	0.31%	0.00%

Fig. 19. Legend

5.3. Odor Sampling

At no time during the demonstration program did the test team receive any complaints about odor originating from the steam plant. Test team members, BAE faculty and staff associated with the project, and the steam plant personnel (10 individuals, in total) monitored the campus for odor and recorded their findings at least twice for each test series. Odor was monitored (36) times throughout the demonstration program. Each odor test began at the steam plant; and, if the wind speed exceeded 1 to 2 mph, was repeated again 0.5 to 1.0 miles down wind of the steam plant. A check of the UGA campus weather website preceding each test confirmed the wind direction and velocity. All odor testers were asked to verify that they were not suffering from any nasal congestion.

Odor was not detected during any of the (17) tests taken down wind of the steam plant. However, there were noticeable fat and grease odors detected in the vicinity (within 100 ft.) of the biofuel tankers.

5.4. Flue Gas Recirculation (FGR) Flow Measurement

Approximately 7 to 10 % of the boiler breaching flue gas was recirculated to the forced draft fan inlet with the recirculation damper 100% open. The test team performed a series of flowrate measurements using standard pitot tube traverse methodology. Measurements were made for all fuels, at both full and part load conditions.

The arrangement of the FGR ducting made pitot traversing difficult and impeded the accuracy of the tests. However, the tests are deemed accurate within 25%, which is sufficient to determine that the system was functioning.

5.5. Discussion

The most significant source of data inaccuracy during the particulate testing is the % of isokinetic sampling, which is the ratio of flue gas flow rate to the sampling flow rate. The GA EPD allows these rates to average within 10% of each other during a one-hour sample period, i.e., a test accuracy of 10%+/- . For compliance testing, two out of three samples must meet the 10% criteria. During this test program, at least one particulate test for each fuel met the EPD requirement.

Odor and opacity test readings were subjective. Their degree of accuracy cannot be documented. Statistical analysis using the Student's t-test statistic was used to test for significant difference ($\alpha = 0.05$) for other data using Sigma-Plot version 2.01 software (Jandel Corporation, San Raphael, CA).

Total particulate emissions from biofuel oil as a group were not significantly different from particulate emissions from #2 fuel oil. However, total particulate emissions from chicken fat fuel was significantly higher than the other biofuel oils and both chicken fat and choice white fat particulate emissions were significantly higher than #2 fuel oil. Particulate emissions from chicken fat fuel were significantly higher than those from choice white grease.

In general, the most significant source of data inaccuracy during gaseous emission testing is the specified 2%+/- accuracy of the ENERAC sensors.

Most of the NO_x formed during combustion is from high temperature oxidation of atmospheric nitrogen. This NO_x is referred to as "thermal NO_x and is popularly modeled as an exponential function of flame temperature and a square root function of oxygen concentration. Thus, the formation of thermal NO_x can be controlled by manipulating the flame temperature or the oxygen concentration (Agrawal and Wood, 2002). Average emissions of NO_x from the combustion of

all biofuel oils were not found to be significantly different than emissions from #2 fuel oil (Student's unpaired t-test, 0.05 significance level). However, the NO_x emissions from chicken fat alone were significantly higher than the other biofuel oils and #2 fuel oil and natural gas. This result is confounding, the chicken fat fuel contained higher ash (Table 3), however, total nitrogen was low and combustion conditions were identical to the other combustion tests.

The procedures used in this testing of FGR both reduced oxygen (which decreases NO_x) and increased furnace temperature (which increases NO_x, see *Fig. 15*, Legend). The net result was that for all cases when flue gas recirculation was used, NO_x decreased in the range of 2.8% to 32.5%, significantly different from emissions without FGR according to a Student's paired t-test ($\alpha = 0.05$). The discrepancy between the factors simultaneously driving the increase and the decrease of NO_x should be further studied.

The ENERAC may have recorded SO₂ readings significantly lower than actual. Gas samples extracted from the breaching were cooled below the SO₂ condensation temperature (to remove excess moisture) before the sample was analyzed by the ENERAC. However, the relative SO₂ data values presented in *Fig. 16* are considered valid because this data is proportional to % sulfur analyzed in the fuels. The biofuel oils had practically zero amounts of SO₂ in emissions and they were significantly less than the biofuel oil blends and #2 fuel oil. Additionally, biofuel oil blends had significantly lower SO₂ emissions than #2 fuel oil.

There were significantly lower CO₂ emissions from biofuel oil versus #2 fuel oil. Additionally, 33% blends of biofuel oil in #2 fuel oil had significantly lower CO₂ emissions.

There was no significant difference in CO emissions between the biofuel oils, blends, or #2 fuel oil. FGR had no significant effect on CO or combustibles emissions. Chicken fat and yellow grease emissions were significantly lower in combustibles than #2 fuel oil.

6. CONCLUSIONS

Fats and greases were demonstrated as industrial boiler fuels. These biofuels easily and economically displace No. 2 fuel oil using the same boiler operating procedures as fuel oil without any modifications to internal boiler combustion equipment. The biofuels need to be kept warm during cold weather in order to flow through piping and equipment. When heated to about 160° F. biofuels are easily atomized and ignited. Construction costs for the pump, heat exchanger, instruments, piping, valves, fittings, and electrical system for a system to maintain the 160° F. temperature and to transfer fuel from storage to the boiler was less than \$31,000. This total does not include the cost of engineering or the procurement cost for the heat exchanger. Extra costs would be incurred if separate storage tanks were needed for biofuel storage. Research should be accomplished focusing on the issues associated with using existing No. 2 fuel oil storage tanks for the storage of biofuel and biofuel blends.

Air emissions from the combustion of the biofuel oils met or exceeded state and federal air quality permit requirements for The University of Georgia. Nitrogen oxides and particulate emissions were comparable to emissions from the combustion of No. 2 fuel oil, Table 4. Sulfur dioxide emissions and deposits on boiler tubes were similar to those encountered when burning natural gas. Biofuels also have low carbon monoxide emissions. The fuel nozzle used in the UGA boiler was a 1950's design and no special procedures were used to minimize emissions through nozzle placement. Flue gas recirculation (FGR) was tested with 7% to 10% of flue gas being recirculated. FGR did not significantly increase boiler efficiency but did significantly reduce NO_x emissions compared to tests without FGR according to a Students t-test at the $\alpha = 0.05$ significance level. NO_x emissions were not reduced enough to meet regulations for new sources and for non-attainment areas. Additional testing is required using low NO_x nozzle designs and other methods for minimizing emissions. When the boiler was operated at half load, boiler efficiency was significantly greater for a blend of 33% tallow with 77% #2 fuel oil than when using 100% #2 fuel oil ($\alpha = 0.05$).

The biofuel oils have high heating value; low amounts of ash, nitrogen, and moisture; and negligible amounts of sulfur. Heating values of the biofuel oil blends tested are within 95% of the heating value of No. 2 fuel oil. The specific gravity of the biofuels is close to that of No. 2 fuel oil. The biofuels are more viscous than No. 2 fuel oil, but much less viscous than No. 6 fuel oil. However, a blend of 30% biofuel with No. 2 fuel oil has a viscosity that is close to that of No. 2 fuel oil. Boiler efficiency while burning biofuel oil is comparable to that of No. 2 fuel oil.

Table 5, Comparison of UGA Test Emissions to US EPA Criteria Pollutant Emission Factors

Fuel & Firing Condition	NO _x , lb./MMBtu	Filterable PM, lb./MMBtu	CO, lb./MMBtu	SO ₂ , lb./MMBtu ⁵
UGA Boiler No. 2 Emissions, Tested at Max. Steam Load¹:				
Chicken Fat, controlled with FGR ⁷	0.156	0.077	0.008	0.000
Yellow Grease, controlled with FGR ⁷	0.097	0.009	0.016	0.001
Choice White Grease, controlled with FGR ⁷	0.150	0.038	0.014	0.000
Tallow, controlled with FGR ⁷	0.101	0.014	0.018	0.007
No. 2 Fuel Oil, controlled with FGR ⁷	0.116	0.010	0.004	0.219
UGA Boiler No. 2 Emissions, Estimated at Max. Steam Load²:				
Chicken Fat, uncontrolled (w/o LNB or FGR)	0.164	not available	0.000	0.000
Yellow Grease, uncontrolled (w/o LNB or FGR)	0.127	not available	0.012	0.000
Choice White Grease, uncontrolled (w/o LNB or FGR)	0.154	not available	0.014	0.000
Tallow, uncontrolled (w/o LNB or FGR)	0.118	not available	0.012	0.002
No. 2 Fuel Oil, uncontrolled (w/o LNB or FGR)	0.125	not available	0.003	0.150
Chicken Fat, blended ⁶ , uncontrolled	0.137	not available	0.008	0.124
Yellow Grease, blended ⁶ , uncontrolled	0.122	not available	not available	0.034
Choice White Grease, blended ⁶ , uncontrolled	0.144	not available	0.012	0.119
Tallow, blended ⁶ , uncontrolled	0.129	not available	0.008	0.102
Chicken Fat, blended ⁶ , controlled w. FGR ⁷	0.125	not available	0.014	0.138
Yellow Grease, blended ⁶ , controlled w. FGR ⁷	0.109	not available	not available	0.083
Choice White Grease, blended ⁶ , controlled w. FGR ⁷	0.138	not available	0.033	0.188
Tallow, blended ⁶ , controlled w. FGR ⁷	0.125	not available	0.008	0.119
US EPA Emission Factors for Criteria Pollutants (boilers > 100 MMBtu/hr heat input)^{3,4}:				
No. 2 Fuel Oil fired, controlled with FGR	0.071	0.014	0.036	0.393
Natural Gas fired, controlled with FGR	0.098	0.002	0.082	0.000
No. 2 Fuel Oil fired, uncontrolled (w/o LNB or FGR)	0.171	0.014	0.036	0.393
Natural Gas fired, uncontrolled (w/o LNB or FGR)	0.186	0.002	0.082	0.000

1) Advanced Air Consultants, Murrayville, GA

2) Emissions data have been estimated using the test results from Advanced Air Consultants and ENERAC 3000E testing.

3) US EPA Fifth Edition 1995, with Supplements: A (1996), B (1996), D (1998), and E (1998)

4) The UGA No. 2 Boiler Operating Permit is based upon a 130 MMBtu/hr heat input.

5) SO₂ emissions data have been reviewed in report Section 5.5, Discussion.

6) All blended fuels consist of 33% biofuel and 67% No. 2 fuel oil.

7) The FGR system was limited to 7% - 10% flue gas recirculation, see report Section 3.4.

Additional research is needed to understand:

1. What is the effect of biofuel/fuel oil blend proportions on viscosity and miscibility? What blend proportions maintain fluidity (low viscosity) over the range of ambient storage temperatures (say, 32 to 100° F.) typical in industrial applications? What is the minimum amount of agitation required?
2. What are minimum required specifications for fats and greases used as biofuel? What are the requirements for solids removal (screening), MIU (moisture, insolubles, unsaponifiables), Ultimate analysis (C, H, N, S), energy content, specific gravity, viscosity, etc.? How shall biofuels be specified for environmental permitting?

7. REFERENCES

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10. Georgia Department of Natural Resources, Environmental Protection Division, Air Protection Branch, Rules for Air Quality Control Chapter 391-3-1, effective December 26, 2001.
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Air Emissions Test Report

For

Boiler Number 2

Animal Fats

Engineering Trials

At

UGA Steam Plant

Athens, Georgia

January 30 - February 8, 2002

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APPENDIX

Test Calculations
Laboratory Data
Field Data
Calibration Data

INTRODUCTION

Emission testing for condensible and non-condensable particulate was conducted at The University of Georgia Steam Plant located in Athens, Georgia. The exhaust from the Number 2 Boiler was tested to demonstrate the feasibility of burning animal fats as a source of fuel. The tests were conducted between January 30 and February 8, 2002. Two test runs, each conducted under normal operation, were performed on each of five different fuels.

The particulate emissions tests were performed by Advanced Air Consultants Inc. under the leadership of Bill Timpone, President. Simultaneously with the particulate tests, UGA Engineering Outreach students performed testing for carbon monoxide, nitrogen oxides, sulfur dioxide, oxygen, and carbon dioxide. The tests were coordinated by Bob Synk, P.E. of Project Management Resources, and Dr. Tom Adams, UGA Engineering Outreach Program.

SUMMARY OF RESULTS

The summary of test results is shown on the following page. The basic gas parameters are given as well as the various pollutant emission rates. The particulate mass concentrations and emission rates are given in terms of the condensible, non-condensable, and total emissions. All of the supporting data and calculations are included in the appendix.

The particulate mass concentration was calculated by dividing the particulate mass collected by the dry standard volume of gas sampled. The product of the mass concentration and the dry standard gas flow rate yielded the mass emission rate in pounds per hour. The product of the mass concentration, the EPA F-Factor, and an excess air correction factor yielded the mass emission rate in pounds per million BTU of heat input. Measurements made by UGA staff yielded ppm volume concentrations of carbon monoxide, nitrogen oxides, and sulfur dioxide. The volume concentrations were converted to mass concentrations and multiplied by the dry standard gas flow rate to obtain the mass emission rates in pounds per hour. The F-Factor was used to calculate the emission rate in pounds per million BTU as for the particulate results.

The F-Factor method of calculating emission rates was developed by the US EPA. The F-Factor is the ratio of dry gas generated per million BTU of heat input for a given fuel. F-Factors for various fuels were determined and tabulated in EPA Method 19 contained in 40CFR60. The F-Factors for the various fuels burned during this project were calculated using equations provided

in Method 19 combined with fuel analysis of samples collected by UGA.

TEST METHODS AND PROCEDURES

The tests were conducted according to reference methods developed by the EPA and promulgated in the Code of Federal Regulations, Title 40, Parts 51 and 60. A brief description of each of the methods used is given below. All of the test equipment was manufactured and calibrated as specified in the reference methods. Calibration data is included in the Appendix.

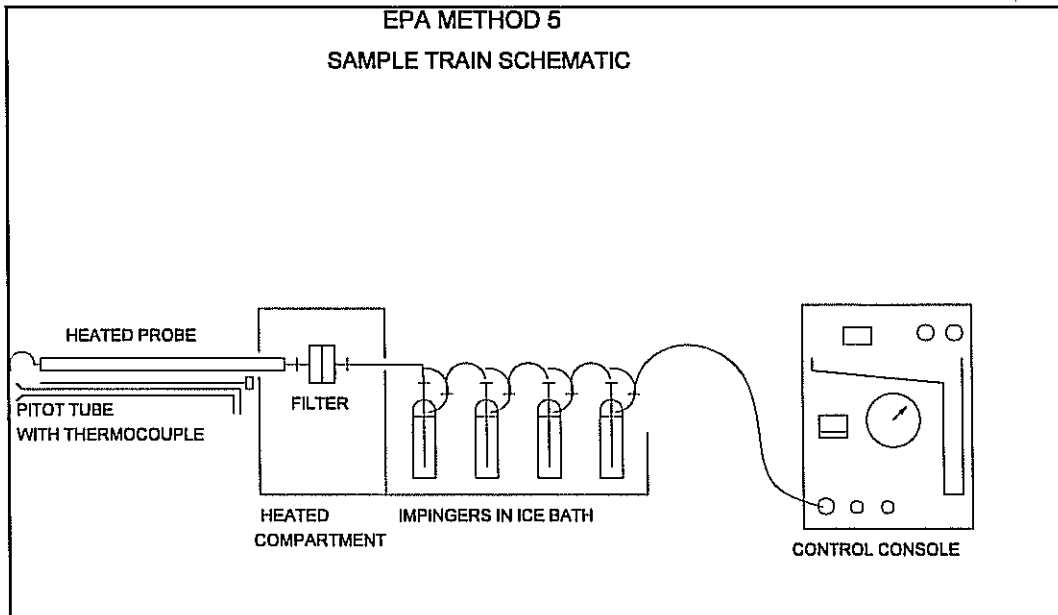
The number of velocity traverse points was chosen based on the distance of the test ports from up and downstream flow disturbances. Twenty total traverse points were sampled. The test location was in a straight section of duct between the boiler and a combined boiler stack. Flow disturbances were located 2.5 diameters upstream and 1.0 diameters downstream from the test ports. The duct interior was 48.5 inches deep by 62 inches high. Test ports were located at 6.2, 18.6, 31, 43.4, and 55.8 inches from the top of the duct. Traverse points were located at 6.1, 18.2, 30.3, and 42.4 inches from the duct sidewall.

EPA Method 2 was used to determine the average gas velocity and volumetric flow rate. The gas velocity pressures were measured using a "S" type pitot tube and an inclined manometer. A type K thermocouple and a digital thermometer were used to measure the gas temperature.

The gas dry molecular weight was measured using EPA Method 3. The grab sampling technique was used and the gas was analyzed with Fyrite Analyzers. Oxygen concentrations used to

calculate the F-Factor based emission rates were obtained from UGA test data.

The moisture was determined by measuring the moisture collected in the particulate impinger



train as outlined in EPA Method 4.

The particulate concentration in the exhaust was measured using an EPA Method 5 sampling train. The sample train consisted of a stainless steel nozzle, stainless steel union, stainless steel lined probe, glass filter holder with teflon filter support, four glass impingers, umbilical cord, vacuum pump, dry gas meter and orifice. Both the probe and filter compartment were heated to 250 degrees Fahrenheit. The impingers were placed in an ice bath to remove moisture from the sample gas stream. All sample exposed impingers were of the screw-joint/O-ring design. This eliminated the necessity of using vacuum grease to seal the impinger joints. The vacuum grease is a possible source of sample contamination when recovering the sample with methylene

chloride as required by this method.

In preparation, the glassware was washed with hot soapy water followed by a water rinse. The glassware was then rinsed with deionized water, acetone, and methylene chloride, and allowed to air dry. All potential contamination openings were sealed until sampling.

The sampling train was assembled on site prior to testing. A filter holder containing a clean, pre-weighed filter was placed in the filter compartment. In each of the first two impingers was placed 100 ml of deionized ultra filtered (DIUF) water. The third impinger was left empty, and the fourth contained 200 grams of silica gel. After the train was assembled, a leak check was conducted.

To begin testing, the probe tip was placed at the first sampling point. The pump was turned on, and the sampling rate set at the isokinetic rate. The following data was recorded at each traverse point: clock time, vacuum, stack temperature, velocity head, orifice meter differential, gas sample volume, gas meter temperature, probe temperature, filter holder temperature, and last impinger exit temperature. Each of the sample traverse points was sampled for three minutes, recording the above data at the beginning of each interval. The total sampling period for each of the three test runs was sixty minutes. At the end of the sampling period, the pump was turned off to end the test run. A post test leak check was conducted to validate the run.

The sampling train was disassembled to recover the sample. The filter holder was disconnected and both ends capped. The filter was recovered indoors to prevent sample loss or contamination. The probe nozzle was separated from the probe liner and rinsed and brushed using acetone. The probe liner was likewise rinsed and brushed using acetone. The acetone rinse from both the nozzle and probe washing was stored in a labeled glass bottle.

The condensible particulate recovery began by measuring the liquid in each of the first three impingers. The liquid was then placed in a clean, labeled polyethylene sample bottle. Each impinger and the connecting glassware was rinsed with DIUF water and the rinse added to the same sample bottle. Next the impingers and connecting glassware were rinsed with methylene chloride and the rinse stored in a clean, labeled glass sample bottle. The silica gel from the fourth impinger was stored in its original labeled container. Each sample train was reassembled as before to start another test run. A blank was taken of the acetone, DIUF water, and methylene chloride for analysis with the samples.

Each filter was recovered at the AAC laboratory. The filter was removed from the filter holder and stored in a clean, labeled petri dish. The front half of the filter holder was rinsed and brushed using acetone. The rinse was collected and stored in the acetone probe wash bottle for that test run. The back half of the filter holder was rinsed and brushed using methylene chloride

and the rinse saved along with the impinger⁸ rinse for that run.

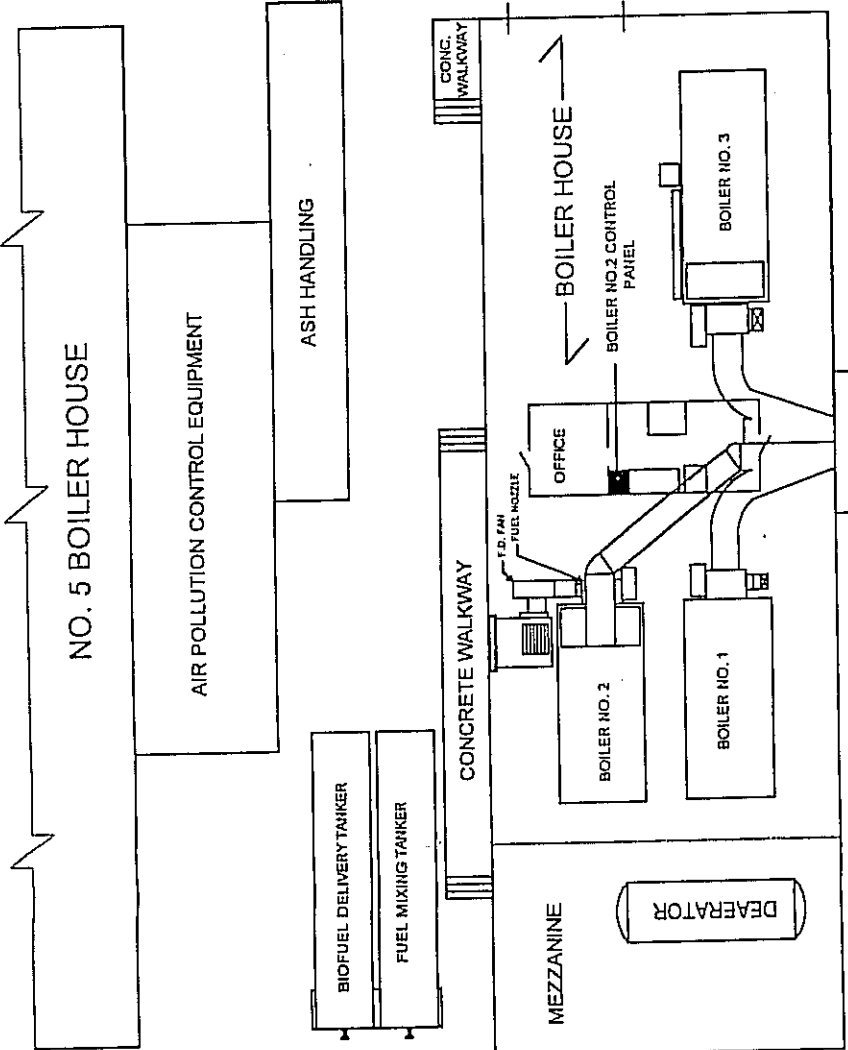
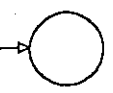
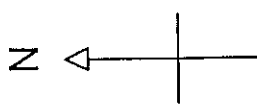
The analysis of the non-condensable particulate sample was performed according to EPA Method 5. The acetone probe wash was evaporated in a tared glass beaker, and the residue desiccated for 24 hours, then weighed to constant weight. The filter was desiccated for 24 hours and weighed to constant weight.

The condensable particulate sample was analyzed according to EPA Method 202. The methylene chloride rinse was added to the impinger water in a 1000 ml separatory funnel. After mixing, the aqueous and organic phases were allowed to fully separate. The organic/methylene chloride phase was drained off. 75 ml of clean methylene chloride was added to the water in the funnel and the process repeated. The process was repeated a third time with another 75 ml of methylene chloride which should have yielded an approximate total of 250 ml of organic extract. The extract was placed in a tared beaker for weighing.

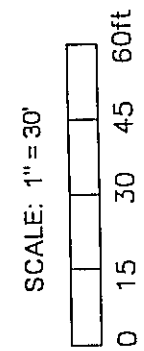
The organic extract was evaporated at ambient temperature and pressure under a laboratory hood. Then it was desiccated for 24 hours and weighed to constant weight.

The inorganic condensable particulate sample was also analyzed by EPA Method 202. The impinger water was evaporated to near dryness in a laboratory oven. It was then allowed to dry at ambient temperature and pressure. The sample was desiccated for 24 hours and weighed to constant weight. The silica gel was weighed to the nearest 0.1 gram.

All weighings for the particulate samples were performed on a Denver Instruments Model A-250 analytical balance in the AAC laboratory. Advanced Air Consultants has been certified per NELAC procedures for the Method 5 analytical method. ASTM Class 1 weights were weighed with the samples to validate the balance accuracy.



NOTES: 1) ELEVATIONS:
 ALLEY, TOP TO CONCRETE: 0'-0"
 DIKED AREA, TOP OF CONCRETE: 0'-7"
 BOILER HOUSE FLOOR: 2'-4"
 BOILER NO. 2 BURNER: 8'-10"

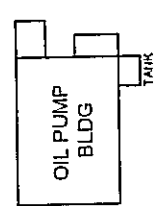


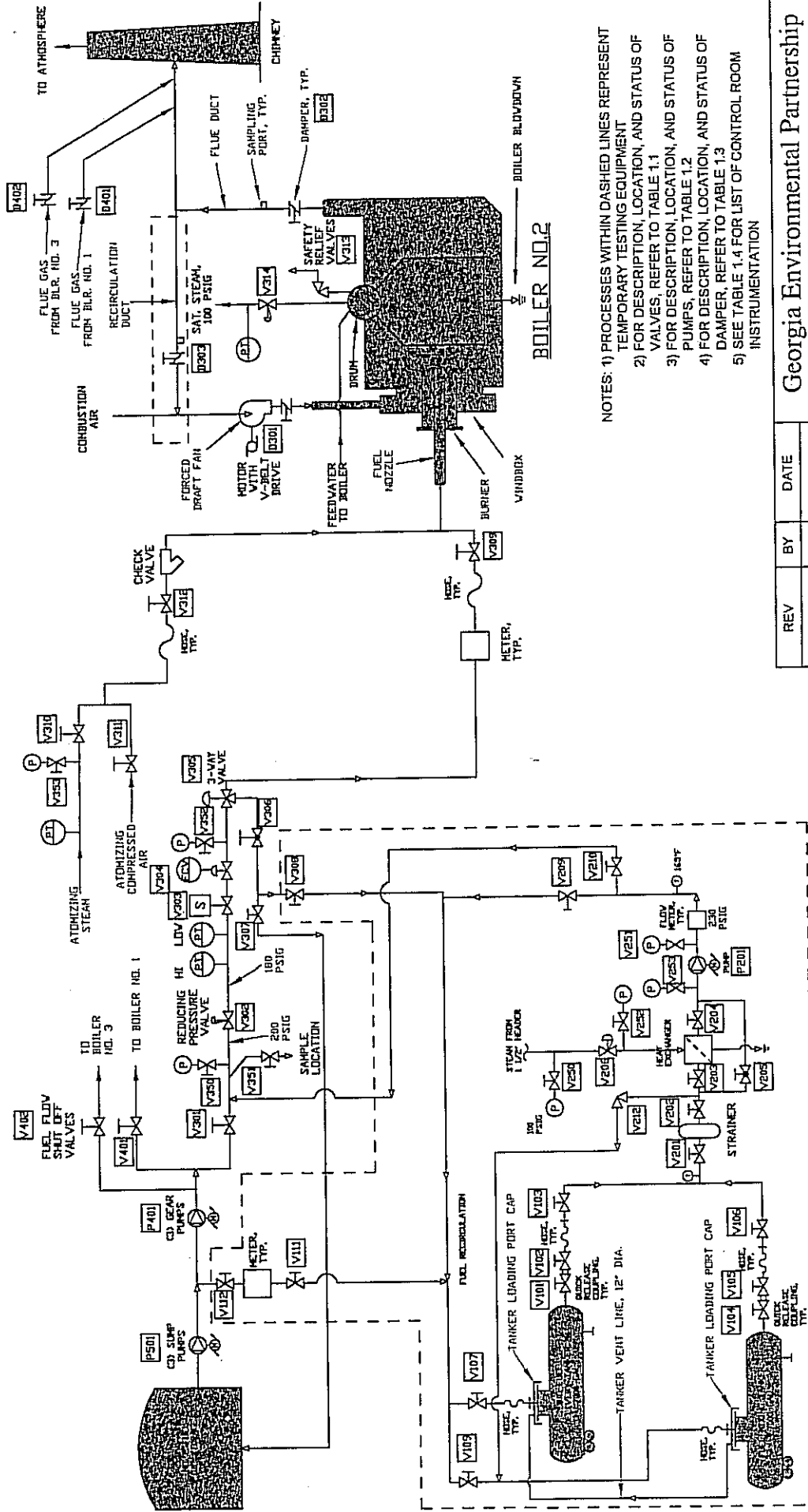
REV.	BY	DATE
A	HZ	6/21/01

DRAWN BY: HZ		DATE: 5/11/01
DESIGNED BY: RS		DATE: 5/11/01

Georgia Environmental Partnership
 THE DEMONSTRATION OF CHICKEN FAT AS AN
 INDUSTRIAL BOILER FUEL
 THE UNIVERSITY OF GEORGIA
 CENTRAL STEAM PLANT SITE PLAN

DWG. NO SK-001





BOILER NO. 2

- NOTES: 1) PROCESSES WITHIN DASHED LINES REPRESENT TEMPORARY TESTING EQUIPMENT
 2) FOR DESCRIPTION, LOCATION, AND STATUS OF VALVES, REFER TO TABLE 1.1
 3) FOR DESCRIPTION, LOCATION, AND STATUS OF PUMPS, REFER TO TABLE 1.2
 4) FOR DESCRIPTION, LOCATION, AND STATUS OF DAMPER, REFER TO TABLE 1.3
 5) SEE TABLE 1.4 FOR LIST OF CONTROL ROOM INSTRUMENTATION

REV	BY	DATE
A	HZ	6/21/01
B	HZ	7/12/01

Georgia Environmental Partnership
 THE DEMONSTRATION OF CHICKEN FAT AS AN INDUSTRIAL BOILER FUEL
 THE UNIVERSITY OF GEORGIA
 MODIFIED PROCESS FLOW DIAGRAM
 DRAWN BY: HZ DATE: 5/11/01
 DESIGNED BY: RS DATE: 5/11/01

NO SCALE

DWG. NO. SK-004

MATERIAL DATA SHEET

IDENTITY	Poultry Fat\ Yellow Grease\Feed Fat\Brown Grease
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Chemical Family	Triglycerides
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SECTION I

Manufacturer's Name American Proteins, Inc. 4705 Leland Drive Cumming, Georgia 30041	Emergency Telephone Number 770-886-2250 Telephone Number for Information: Date Prepared:
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SECTION II - HAZARDOUS INGREDIENTS\IDENTITY INFORMATION

Hazardous Components	Not Applicable
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SECTION III - PHYSICAL\CHEMICAL CHARACTERISTICS

Boiling Point	NA	Specific Gravity (H2O=1)	.89@140F
Vapor Pressure (mmHg)	NA	Melting Point	50-105F
Vapor Density (air=1)	NA	Evporation Rate (Butyl Acetate=1)	NA
Solubility in Water	None White to Brown Liquid		
Appearance and odor			

SECTION IV - FIRE AND EXPLOSION HAZARD DATE

Flash Point	550F	Flammable Limits	NA
Extinguishing Media	Class B Fire, CO2, Foamite		
Special Fire Fighting Procedures	Same as Oil Fire, use no water		
Unusual Fire and Explosion Hazards	Aerosol in container under high heat could present an explosion hazard.		

SECTION V - REACTIVITY DATA

Stability	Unstable	NA	Conditions to Avoid
	Stable		
Incompatibility (Materials to Avoid)	NA	Avoid Oxidants	
Hazardous Decomposition or Byproducts	NA	Avoid high temperature	
Hazardous Polymerization	May Occur		
	Will Not Occur		X

SECTION VI - HEALTH HAZARD DATA

Routes of Entry	Inhalation	Skin	Ingestion
Health Hazards (Acute and Chronic)	NA	NA	NA
Carcinogenicity	NA	NA	NA
Signs and Symptoms of Exposure	NA	NA	NA
Medical Conditions Aggravated by Exposure	NA	NA	NA
Emergency and First Aid Procedures	NA	NA	NA

SECTION VII - PRECAUTIONS FOR SAFE HANDLING AND USE

Steps to be taken in case Material is Released or Spilled	
Will solidify at ambient temperature if liquid is contained, may be shoveled up.	
While liquid it may be mopped, soaked up in absorbents or pumped.	
Waste Disposal Method	
Totally Biodegradable. Use sealed drums or vacuum to pump liquid when contaminated.	
Precaution to be taken in Handling and Storing	
Avoid skin contact with hot liquid to prevent burns.	
Other Precautions	

SECTION VIII - CONTROL MEASURES

Respiratory Protection (Specify type)		NA	
Ventilation	Local Exhaust	Special	
	Mechanical (General)	Other	
Protective Gloves	Use to Avoid	Eye Protection	Use goggles to avoid splashes.
Contact with hot liquid.			
Other Protective Clothes or Equipment			
Work Hygienic Practices			

Material Safety Data Sheet
Identity: Choice White Grease

Section I - General Information

Manufacturer's Name: Griffin Industries, Inc.
 4221 Alexandria Pike
 Cold Spring, KY 41076

Emergency Telephone Number:
 (806) 472-7363

Telephone Number for Information:
 (806) 472-7363

Date Prepared: 3/23/93
 Signature of Preparer: Eugene M. Weddington

Section II - Hazardous Ingredients/Identity Information

Hazardous Components - Contains no Hazardous Components as described in the Hazard Communication Standard

Substance - Rendered Animal Fat CAS Number N/A

Trade Names - Choice White Grease, Inedible Grease, Animal Fat

Chemical Family: Triglyceride; Triacylglycerol

Molecular Formula: N/A Molecular Weight: N/A

CERCLA Ratings (Scale 0-3): Health = 0 Fire = 2 Reactivity = 0 Persistence = 1

Components and Contaminants

Components: Triglycerides Percent: 100%

Other Contaminants: None Exposure Limits: N/A

Section III - Physical/Chemical Characteristics

Boiling Point: Decomposes Specific Gravity (H₂O = 1): 0.84 avg.

Vapor Pressure (mm Hg): N/A Melting Point: 32.5° C

Vapor Density (Air = 1): N/A Evaporation Rate: 0
 (Butyl Acetate = 1)

Solubility in Water: Insoluble

Appearance and Odor: Yellow liquid to pale brown solid, bland odor

Section IV - Fire and Explosion Hazard Data

Flash Point (Method Used): 525° F, Open Cup

Flammable Limits: N/A LEL: N/A UEL: N/A

Extinguishing Media: Type B (Flammable Liquids)

Special Fire Fighting Procedures: None

Unusual Fire and Explosion Hazards: None

Section V - Reactivity Data

Reactivity: Stable

Conditions to Avoid: None

Incompatibility (Materials to Avoid): None

Hazardous Decomposition or Byproducts: None

Hazardous Polymerization: Will Not Occur

Section VI - Health Hazard Data

Inhalation: N/A

Skin Contact: N/A

Eye Contact: N/A

Ingestion: N/A

Emergency and First Aid Procedures: Wash well, treat for possible heat burns

Carcinogenicity: None NTP? N/A IARC Monographs: N/A

OSHA Regulated: No

Section VII - Precautions for Safe Handling and Use

Steps to be taken in case material is released or spilled -

Contain and contact Griffin Industries, Inc. concerning reprocessing.

Waste Disposal Method - Rendering (reprocessing), not to be landfilled. Do not flush to sewer.

Precautions To Be Taken in Handling and Storing - None

Other Precautions - None

Section VIII - Control Measures

Respiratory Protection - None

Ventilation - Ventilate tanks before entering.

Protective Gloves - Standard

Eye Protection - Standard

Other Protective Clothing or Equipment - Standard

Work/Hygienic Practices - Standard

The information provided is believed to be accurate and represents the best information currently available to us. However, we make no warranty of merchantability or any other warranty, express or implied, with respect to such information, and we assume no liability resulting from its use. Users should make their own investigations to determine the suitability of the information for their particular purposes.

Identity: Tallow**Section I - General Information**

Manufacturer's Name: Griffin Industries, Inc.
4221 Alexandria Pike
Cold Spring, KY 41076

Emergency Telephone Number:
(859) 472-7363
Telephone Number for Information:
(859) 472-7363

Date Prepared: 12/26/00
Preparer: Thomas L. Dobbs

Section II - Hazardous Ingredients/Identity Information

Hazardous Components - Contains no Hazardous Components as described in the Hazard Communication Standard

Substance - Rendered Animal Fat CAS Number N/A

Trade Names - Tallow

Chemical Family: Triglyceride; Triacylglycerol

Molecular Formula: N/A

HMIS Ratings: Health = 0 Fire = 1 Molecular Weight: N/A

Reactivity = 0

Components and Contaminants

Components: Triglycerides Percent: 100%

Other Contaminants: None Exposure Limits: N/A

Section III - Physical/Chemical Characteristics

Boiling Point: Decomposes Specific Gravity (H₂O = 1): 0.84 avg. AT 75 degrees F.

Vapor Pressure (mm Hg): N/A Melting Point: 35° C

Vapor Density (Air = 1): N/A Evaporation Rate: 0

(Butyl Acetate = 1)

Solubility in Water: Insoluble

Appearance and Odor: Light brown liquid to pale brown solid, bland odor

Section IV - Fire and Explosion Hazard Data

Flash Point (Method Used): 410° F, Open Cup

Flammable Limits: N/A LEL: N/A UEL: N/A

Extinguishing Media: Type B (Flammable Liquids)

Special Fire Fighting Procedures: None

Unusual Fire and Explosion Hazards: None

Section V - Reactivity Data

Reactivity: Stable

Conditions to Avoid: None

Incompatibility (Materials to Avoid): None

Hazardous Decomposition or Byproducts: None

Hazardous Polymerization: Will Not Occur

Section VI - Health Hazard Data

Inhalation: N/A

Skin Contact: N/A

Eye Contact: N/A

Ingestion: N/A

Emergency and First Aid Procedures: Wash well, treat for possible heat burns

Carcinogenicity: None NTP IARC Monographs: N/A

OSHA Regulated: No

Section VII - Precautions for Safe Handling and Use

Steps to be taken in case material is released or spilled -

Contain and contact Griffin Industries, Inc. concerning reprocessing.

Waste Disposal Method - Rendering (reprocessing). Do not flush to sewer.

Precautions To Be Taken in Handling and Storing - None

Other Precautions - None

Section VIII - Control Measures

Respiratory Protection - None

Ventilation - Ventilate tanks before entering.

Protective Gloves - Standard

Eye Protection - Standard

Other Protective Clothing or Equipment - Standard

Work/Hygienic Practices - Standard

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